1000 Noble Energy Drive Canonsburg, PA 15317

Tel: 724-820-3000 Fax: 724-820-3098 www.nobleenergyinc.com





October 6, 2016

Ms. Beverly McKeone NSR Permitting Program Manager West Virginia Department of Environmental Protection Division of Air Quality 601 57th Street, SE Charleston, WV 25304

RE: Noble Energy, Inc

SHL 22

45CSR13 Permit Application Marshall County, West Virginia

Dear Ms. McKeone:

Noble Energy, Inc respectfully submits this Air Quality Permit Application for the above referenced facility pursuant to 45CSR13. We look forward to working towards a timely review and issuance of the requested approval.

This application is for the construction and operation of a Marcellus Natural Gas Production Facility located in Marshall County, West Virginia. While condensate and natural gas will be produced directly to pipeline, the proposed design includes control devices for the produced water tanks and loadout as well as a flare for controlling the maintenance / well unloading vessel.

Please find the enclosed information for all associated process equipment and control devices.

Please note that the newspaper notification will be published and the original affidavit will be remitted to the Department promptly upon receipt.

Noble Energy will also be contacting the WVDEP to pay the application fee by credit card. Should you have any questions or require further information the application package, please do not hesitate to contact me (Phil.Schlagel@nblenergy.com, 281-872-3202).

We thank you in advance for your efforts in reviewing this submittal.

Phil Schlagel Air Quality Manager

Noble Energy, Inc

Enclosures:

Sincerel

## Noble Energy, Inc

45CSR13 Permit Application SHL 22 Production Facility

Marshall County, West Virginia

October 2016



#### WEST VIRGINIA DEPARTMENT OF **ENVIRONMENTAL PROTECTION**

#### **DIVISION OF AIR QUALITY**

#### APPLICATION FOR NSR PERMIT AND

601 57th Street, SE Charleston, WV 25304 (304) 926-0475 www.dep.wv.gov/dag		TI		RMIT REVISION TIONAL)
PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF K CONSTRUCTION  MODIFICATION  TELOCATION CLASS I ADMINISTRATIVE UPDATE  AFTER-THE-	N Y FACT	ADMINISTRAT	TIVE AMENDM MODIFICATIO VE IS CHECKI	_
FOR TITLE V FACILITIES ONLY: Please refer to "Title V (Appendix A, "Title V Permit Revision Flowchart") and	d ability to	operate with the o	der to determine changes reque	ne your Title V Revision options ested in this Permit Application.
Sec	ction I.	General		
Name of applicant (as registered with the WV Secreta Noble Energy, Inc.	ary of Stat	,	2. Federal l 73-0785597	Employer ID No. <i>(FEIN):</i>
Name of facility (if different from above): Sand Hill 22 (SHL 22)			4. The applic	cant is the:  ☑OPERATOR ☐ BOTH
5A. Applicant's mailing address: 1000 Noble Energy Drive Canonsburg, PA 15317	10	3. Facility's prese 0 Standiford Ro heeling, WV		ddress:
6. West Virginia Business Registration. Is the applican If YES, provide a copy of the Certificate of Incorpor change amendments or other Business Registration If NO, provide a copy of the Certificate of Authority amendments or other Business Certificate as Attach	ration/Org Certificate //Authorit	ganizatìon/Limit e as Attachment	ed Partnersi A.	hip (one page) including any name
7. If applicant is a subsidiary corporation, please provide	the name	of parent corpor	ration:	
8. Does the applicant own, lease, have an option to buy of the second of	s the San			
<ol> <li>Type of plant or facility (stationary source) to be consadministratively updated or temporarily permitted crusher, etc.);</li> <li>Oil and Natural Gas Production Facility</li> </ol>	d (e.g., coa	modified, relocal al preparation pla	ated, ant, primary	North American Industry     Classification System     (NAICS) code for the facility:     211111
11A. DAQ Plant ID No. (for existing facilities only):  -				SR30 (Title V) permit numbers existing facilities only):
All of the required forms and additional information can be	found und	ler the Permitting	Section of DA	Q's website, or requested by phone.

Page 1 of 4

NSR Title V Perm Revision Application Form (Revision Drm.doc)

OCT 14 2016

OCT 14 2016

WV DEP / DIV OF AIR QUALITY

12A			
cţ.	For Modifications, Administrative Updates or T present location of the facility from the nearest sta		, please provide directions to the
G	For Construction or Relocation permits, please road. Include a MAP as Attachment B.		site location from the nearest state
	From Interstate 70, take Dallas Pike Road Exit (Exit 11), (Dallas Pike Road), and travel Dallas Pike Road approxis Road), make a right onto Stone Church/Sand Hill Road aleft hand turn onto Sand Hill Road and travel approximation and travel 0.1 mile to lease road on left.	mately 4.9 miles to the town of Dallas, make a and travel approximately 1.8 miles to CR 7 (W	a right onto CR 7 (Stone Church/Sand Hi /ye Intersection) – Sand Hill Road, make
12.8	. New site address (if applicable):	12C. Nearest city or town: Dallas, WV	12D. County: Marshall
	. UTM Northing (KM): 0.0509	12F. UTM Easting (KM): 536.136	12G. UTM Zone: 17N
13.	Briefly describe the proposed change(s) at the facil	ity:	
New	construction of oil and natural gas production	facility	
	Provide the date of anticipated installation or char If this is an <b>After-The-Fact</b> permit application, prochange did happen: / /	_	14B. Date of anticipated Start-Up if a permit is granted: 0 2 / 1 7 / 2 0 1 7
14C	Provide a <b>Schedule</b> of the planned <b>Installation</b> of application as <b>Attachment C</b> (if more than one un		units proposed in this permit
15.	Provide maximum projected <b>Operating Schedule o</b> Hours Per Day 24 Days Per Week		ation:
16.	s demolition or physical renovation at an existing fa	acility involved? TYES VO	
17. F	tisk Management Plans. If this facility is subject to	o 112(r) of the 1990 CAAA, or will become	ne subject due to proposed
c	nanges (for applicability help see www.epa.gov/cep	po), submit your <b>Risk Management Pla</b>	n (RMP) to U.S. EPA Region III.
18. <b>F</b>	Regulatory Discussion. List all Federal and State	air pollution control regulations that you	believe are applicable to the
р	roposed process (if known). A list of possible applic	able requirements is also included in Att	achment S of this application
(7	itle V Permit Revision Information). Discuss applica	ability and proposed demonstration(s) of	compliance (if known). Provide this
in	formation as Attachment D.		
	Section II. Additional att	tachments and supporting d	ocuments.
	nclude a check payable to WVDEP – Division of Air 5CSR13).	Quality with the appropriate application	n fee (per 45CSR22 and
20.	nclude a Table of Contents as the first page of yo	ur application package.	
	Provide a <b>Plot Plan,</b> e.g. scaled map(s) and/or ske source(s) is or is to be located as <b>Attachment E</b> (R		erty on which the stationary
r r	ndicate the location of the nearest occupied structure	re (e.g. church, school, business, reside	nce).
	Provide a <b>Detailed Process Flow Diagram(s)</b> show device as <b>Attachment F</b> .	wing each proposed or modified emissio	ns unit, emission point and control
23.	Provide a Process Description as Attachment G.		
t.	Also describe and quantify to the extent possible	all changes made to the facility since the	e last permit review (if applicable).
All o	f the required forms and additional information can be	e found under the Permitting Section of DA	O's website, or requested by phone.

24. Pro	ovide Material Safety Data Sheets	(MSDS) for all materials pr	ocessed, used or produced as Attachment H.
< For	chemical processes, provide a MS	DS for each compound em	tted to the air.
25. Fill	out the Emission Units Table and	provide it as Attachment	l
26. Fill	out the Emission Points Data Su	mmary Sheet (Table 1 and	I Table 2) and provide it as Attachment J.
27. Fill	out the Fugitive Emissions Data	Summary Sheet and provi	de it as Attachment K.
28. Che	eck all applicable Emissions Unit	Data Sheets listed below:	
	Liquid Transfer Operations	☐ Haul Road Emissions	☐ Quarry
☐ Cher	mical Processes	☐ Hot Mix Asphalt Plant	Solid Materials Sizing, Handling and Storage
	crete Batch Plant	Incinerator	Facilities
Grey	Iron and Steel Foundry	☐ Indirect Heat Exchang	er Storage Tanks
☑ Gene	eral Emission Unit, specify Pneur	matic Controllers, Fuel C	ell Generator, Diaphragm Pump
Fill out a	and provide the Emissions Unit D	ata Sheet(s) as Attachmer	it L.
29. Che	eck all applicable Air Pollution Co	ntrol Device Sheets listed	below:
☐ Abso	rption Systems	☐ Baghouse	☑ Flare
Adso	rption Systems	Condenser	
☐ After	<del></del>	☐ Electrostatic Prec	pitator
☑ Othe	r Collectors, specify NSCR		
Fill out a	and provide the Air Pollution Cont	rol Device Sheet(s) as Att	achment M.
30. Pro	vide all <b>Supporting Emissions Ca</b> ns 28 through 31.	alculations as Attachment	N, or attach the calculations directly to the forms listed in
test	nitoring, Recordkeeping, Report ing plans in order to demonstrate o lication. Provide this information a	compliance with the propose	each proposed monitoring, recordkeeping, reporting and and emissions limits and operating parameters in this permit
mea	ase be aware that all permits must asures. Additionally, the DAQ may proposed by the applicant, DAQ w	not be able to accept all me	whether or not the applicant chooses to propose such easures proposed by the applicant. If none of these plans include them in the permit.
32. Pub	lic Notice. At the time that the ap	pplication is submitted, place	e a Class I Legal Advertisement in a newspaper of general
circu	ulation in the area where the sourc	e is or will be located (See	ISCSR§13-8.3 through 45CSR§13-8.5 and Example Legal
Adv	rertisement for details). Please su	bmit the Affidavit of Publi	cation as Attachment P immediately upon receipt.
33. <b>Bus</b>	iness Confidentiality Claims. Do	oes this application include	confidential information (per 45CSR31)?
segi	ment claimed confidential, includin	g the criteria under 45CSR	submitted as confidential and provide justification for each 31-4.1, and in accordance with the DAQ's "Precautionary ral Instructions as Attachment Q.
	Sec	tion III. Certification	n of Information
34. Aut	hority/Delegation of Authority. (	Only required when someon	e other than the responsible official signs the application.
☐ Autho	prity of Corporation or Other Busine	ess Entity	☐ Authority of Partnership
	ority of Governmental Agency		☐ Authority of Limited Partnership
Submit o	completed and signed Authority Fo	orm as Attachment R.	-
			he Permitting Section of DAQ's website, or requested by phone.
	· · · · · · · · · · · · · · · · · · ·		by phone.

35A. Certification of Information. To certify 2.28) or Authorized Representative shall chec	this permit application, a Responsible Offick the appropriate box and sign below.	cial (per 45CSR§13-2.22 and 45CSR§30-
Certification of Truth, Accuracy, and Comp	leteness	
I, the undersigned PResponsible Official / application and any supporting documents appreasonable inquiry I further agree to assume restationary source described herein in accorda Environmental Protection, Division of Air Qual and regulations of the West Virginia Division of business or agency changes its Responsible on the official of the official	pended hereto, is true, accurate, and complesponsibility for the construction, modificating with this application and any amendme ity permit issued in accordance with this application and Section 22-5-1 et secondarion of Authorized Representative, the D	lete based on information and belief after on and/or relocation and operation of the nts thereto, as well as the Department of plication, along with all applicable rules eq. (State Air Pollution Control Act). If the
	fer reasonable inquiry, all air contaminant	DATE: (Please use blue ink)
35B. Printed name of signee: RJ Moses		35C. Title: Operations Manager
35D. E-mail: rj.moses@nblenergy.com	36E. Phone: 724-820-3000	36F. FAX: 724-820-3098
36A. Printed name of contact person (if differe Phil Schlagel	nt from above):	36B. Title: Air Quality Manager
36C. E-mail:	36D. Phone:	36E. FAX:
phil.schlagel@nblenergy.com	281-872-3202	
PLEASE CHECK ALL APPLICABLE ATTACHMEN  Attachment A: Business Certificate  Attachment B: Map(s)  Attachment C: Installation and Start Up Sche  Attachment D: Regulatory Discussion  Attachment E: Plot Plan  Attachment F: Detailed Process Flow Diagrar  Attachment G: Process Description  Attachment H: Material Safety Data Sheets (N  Attachment I: Emission Units Table  Attachment J: Emission Points Data Summar  Please mail an original and three (3) copies of the  address listed on the first	Attachment K: Fugitive E Attachment L: Emissions dule Attachment M: Air Polluti Attachment N: Supportin Attachment O: Monitorin n(s) Attachment P: Public Not Attachment Q: Business ISDS) Attachment R: Authority Attachment S: Title V Per y Sheet  Attachment Fee	imissions Data Summary Sheet S Unit Data Sheet(s) S Unit Data Sheet(s) S Unit Data Sheet(s) S Emissions Calculations S (Recordkeeping/Reporting/Testing Plans Stice Confidential Claims Forms The Revision Information  Ure(s) to the DAQ, Permitting Section, at the
FOR AGENCY USE ONLY - IF THIS IS A TITLE V		
☐ Forward 1 copy of the application to the Title ☐ For Title V Administrative Amendments: ☐ NSR permit writer should notify Title V ☐ For Title V Minor Modifications: ☐ Title V permit writer should send appr ☐ NSR permit writer should notify Title V ☐ For Title V Significant Modifications processes ☐ NSR permit writer should notify a Title V ☐ Public notice should reference both 4 ☐ EPA has 45 day review period of a dra  All of the required forms and additional informat	/ permit writer of draft permit, opriate notification to EPA and affected state / permit writer of draft permit. d in parallel with NSR Permit revision: e V permit writer of draft permit, 5CSR13 and Title V permits, ft permit.	
	The state of the s	the state of the state of priorie.



#### **TABLE OF CONTENTS**

#### Attachments:

- A Current Business Certificate
- B Area Map
- D Regulatory Discussion
- E Plot Plan
- F Process Flow Diagram
- **G** Process Description
- I Emission Units Table
- J Emission Points Data Summary Sheet
- K Fugitive Emissions Data
- L Emission Unit Data Sheets
- M Air Pollution Control Device Sheets
- N Supporting Emissions Calculations & Documents
- P Public Notice

Noble Energy, Inc. SHL 22 Production Facility

### Permit Application Fee

As stated in the cover letter, please contact Phil Schlagel (Phil.Schlagel@nblenergy.com, 281-872-3202) for payment.

#### ATTACHMENT A

Noble Energy, Inc.

Certificate of Authority for West Virginia

# Frate of Mest Virginia Certificate

I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

by the provisions of the West Virginia Code, Articles of Merger were received and filed, MERGING NOBLE ENERGY MARKETING, INC., A QUALIFIED DE ORGANIZATION, WITH AND INTO NOBLE ENERGY, INC., A QUALIFIED DE ORGANIZATION.

Therefore, I hereby issue this

**CERTIFICATE OF MERGER** 



Given under my hand and the Great Seal of the State of West Virginia on this day of December 15, 2010

Water E Lemment

State of Delaware Secretary of State Division of Corporations Delivered 06:59 PM 12/17/2009 FILED 06:59 PM 12/17/2009 SRV 091114165 - 0738126 FILE

#### CERTIFICATE OF MERGER OF

NOBLE ENERGY MARKETING, INC.
(a Delaware corporation)
WITH AND INTO
NOBLE ENERGY, INC.
(a Delaware corporation)

Pursuant to Title 8, Section 251(c) of the Delaware General Corporation Law, the undersigned corporation hereby certifies the following:

- The name of the surviving corporation is Noble Energy, Inc., a Delaware corporation, and the name of the corporation being merged into the surviving corporation is Noble Energy Marketing, Inc., a Delaware corporation.
- The Agreement of Merger has been approved, adopted, certified, executed, and acknowledged by each of the constituent corporations.
- 3. The name of the surviving corporation is Noble Energy, Inc., a Delaware corporation.
- The Certificate of Incorporation of Noble Energy, Inc. shall be the Certificate of Incorporation of the surviving corporation.
- The merger is to become effective at 11:59 p.m. Eastern time on December 31, 2009.
- A copy of the Agreement of Merger is on file at the place of business of Noble Energy, Inc., which is located at 100 Glenborough Drive, Suite 100, Houston, Texas 77067.
- Upon request, a copy of the Agreement of Merger will be furnished by Noble Energy, Inc., without cost, to any stockholder of the constituent corporations.

IN WITNESS WHEREOF, the undersigned has caused this Certificate of Merger to be executed by its duly authorized officer as of the 16th day of December, 2009.

NOBLE ENERGY, INC.

By: /s/ David L. Stover Name: David L. Stover Title: Vice President

# Delaware PAGE 1

#### The First State

I, JEFFREY W. BULLOCK, SECRETARY OF STATE OF THE STATE OF DELAWARE, DO HEREBY CERTIFY THE ATTACHED IS A TRUE AND CORRECT COPY OF THE CERTIFICATE OF MERGER, WHICH MERGES:

"NOBLE ENERGY MARKETING, INC.", A DELAWARE CORPORATION, WITH AND INTO "NOBLE ENERGY, INC." UNDER THE NAME OF "NOBLE ENERGY, INC.", A CORPORATION ORGANIZED AND EXISTING UNDER THE LAWS OF THE STATE OF DELAWARE, AS RECEIVED AND FILED IN THIS OFFICE THE SEVENTEENTH DAY OF DECEMBER, A.D. 2009, AT 6:59 O'CLOCK P.M.

AND I DO HEREBY FURTHER CERTIFY THAT THE EFFECTIVE DATE OF THE AFORESAID CERTIFICATE OF MERGER IS THE THIRTY-FIRST DAY OF DECEMBER, A.D. 2009, AT 11:59 O'CLOCK P.M.

FILED

DEC 1 5 2010

IN THE OFFICE OF SECRETARY OF STATE

0738126 8100M

101192174

You may varify this certificate online at corp. delaware.gov/authver.shtml

AUTHENTICATION: 8430215

DATE: 12-15-10





### I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

#### NOBLE ENERGY MARKETING, INC.

Control Number: 99D1Z

a corporation formed under the laws of Delaware has filed its "Application for Certificate of Authority" to transact business in West Virginia as required by the provisions of the West Virginia Code. I hereby declare the organization to be registered as a foreign corporation from its effective date of January 29, 2009.

Therefore, I issue this

# CERTIFICATE OF AUTHORITY

to the corporation authorizing it to transact business in West Virginia



Given under my hand and the Great Seal of the State of West Virginia on this day of January 29, 2009

Natelil E Jermant

Stamper

# FILED

JAN 2 9 2009

Madalia E. Tourous State Capitol 1900 Kasuwia Bivd. E. Chadadon, WY 25305 FILE ONE ORIGINAL FERS PER SCHEDULE

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IN THE OFFICE OF
SECRETARY OF STATE
VEST VIRGINIA Procesy Budget, Minager
Corporations Division
Tel. (104) 558-8000
Per (104) 558-8001
Per (104) 5

CERTIFICATE OF **AUTHORITY** 

		C, MAC 1
1. 1	SOME STATE INPORMATION:	
	The series of the corporation at It is registered in its home state in:	Nobie Energy Marketing, Inc.
b.		Continuery 18, 1894 Despites (6 yes or propolets) Polypolenii  Worshap Tax reporting requirements in West Va- edit and and an elitherareal in Stant.
c.	NASCE	(If an impartment company)
2.	FERNCIPAL OFFICE INFORMATION:	1 T. C. D. M. 488
	Address of the prioripal office of the surpossition	No. & Street  100 Glenberough Drive. Suits 100  Houston, TX 77067
b.	Mailing address; if different, faces shows address:	BenditO Bes Citydines(s)
3.	WEST VIRGINIA INFORMATION	
86	Corporate messe to be used to W. Vil.: Cabate can, follow betweenst	House state mante to tieted on time 1.s. above, if everlable.  DBA neces
b.	Address of registered office in West Vingbein, if any	No. & Bonst 2077 Virginia Stream East Charlecton, WV 25901
c	healing addens in WV, If different, from above	Street/FO Best City/Flate/Zip
d	Proposed purpose(s) for transcation of bostness in WV	Ol & gas
4.	AGENT OF PROCESS: Properly designated person to when notice of process may be sent if sent	Nexus C T Corporation System  Address 707 Virginia Street East, Charleston, WV 25501

S.	CORP	POTAMEDER BUTATE STADO				
	E.	Corporation is organized as (check one):	V	Per profit		
				Hos-profit		
	b.	Obvestors and Officers: (Add extra page if nee	nery; ple	ee list all efform)		
		Officer Name			Adher	
	Plas	se see attacked list.		<u> </u>		
					None	
6.	The	number of some of land it holds or supe	ris to bol	d in Wort Vingis		
			nd of etc	d in West Virgin	ie is:	
ć. 7.		tact and Signature Information.	nd of etc	d in West Virgin	ia is:	
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	Carr	tact med Bigmitture Telforephties. Junit Pages			in is:	28).573,21(9)

# NOBLE ENERGY MARKETING, INC. 6 Delivers corporation

#### Directors

Charles D. Davidson 100 Glenborough Drive, Staits 100 Houston, Texas 77067

Chria Tong 100 Glenborough Drive, Suite 100 Houston, Texas 77067

Amold J. Johnson 100 Glenbarough Drive, Suite 100 Houston, Texas 77067

#### Officers

Name	Title(s)	Address
Charles D. Davidson	Chief Executive Officer	100 Glenborough Drive, Suite 100 Houston, Tures 77067
Devid L. Stower	Vice President	100 Glenborough Drive, Suite 100 Houston, Texas 77067
Amold J. Johnson	Vice President, General Coursel, and Secretary	100 Glenborough Drive, Suite 100 Houston, Texas 77067
Chris Tong	Vice President - Pinence and Treasurer	100 Clemborough Drive, Suite 100 Houston, Texas 77067
Kirk A. Moore	Assistant Socrotary	100 Clemborough Drive, Suite 100 Houston, Texas 77067

0404372 0032214 FEDERATOR SCENIS-3

# Delaware\_ PAGE 1

#### The First State

I, JEFFREY W. BULLOCK, SECRETARY OF STATE OF THE STATE OF DELAWARE, DO HEREBY CERTIFY "NOBLE ENERGY MARKETING, INC." IS DULY INCORPORATED UNDER THE LAWS OF THE STATE OF DELAWARE AND IS IN GOOD STANDING AND HAS A LEGAL CORPORATE EXISTENCE SO FAR AS THE RECORDS OF THIS OFFICE SHOW, AS OF THE TWENTY-NINTH DAY OF JANUARY, A.D. 2009.

AND I DO HEREBY FURTHER CERTIFY THAT THE SAID "MOBILE ENERGY MARKETING, INC." WAS INCORPORATED ON THE EIGHTEENTH DAY OF JANUARY, A.D. 1994.

AND I DO HEREBY FURTHER CERTIFY THAT THE ANNUAL REPORTS HAVE BEEN FILED TO DATE.

AND I DO HEREBY FURTHER CERTIFY THAT THE FRANCHISE TAXES HAVE BEEN PAID TO DATE.

2372438 8300

090081032

You may varify this cartificate colin at corp.delaware.gov/suthwar.shtml

DATE: 01-29-09

Noble Energy, Inc SHL 22 Production Facility Permit G70-A Application

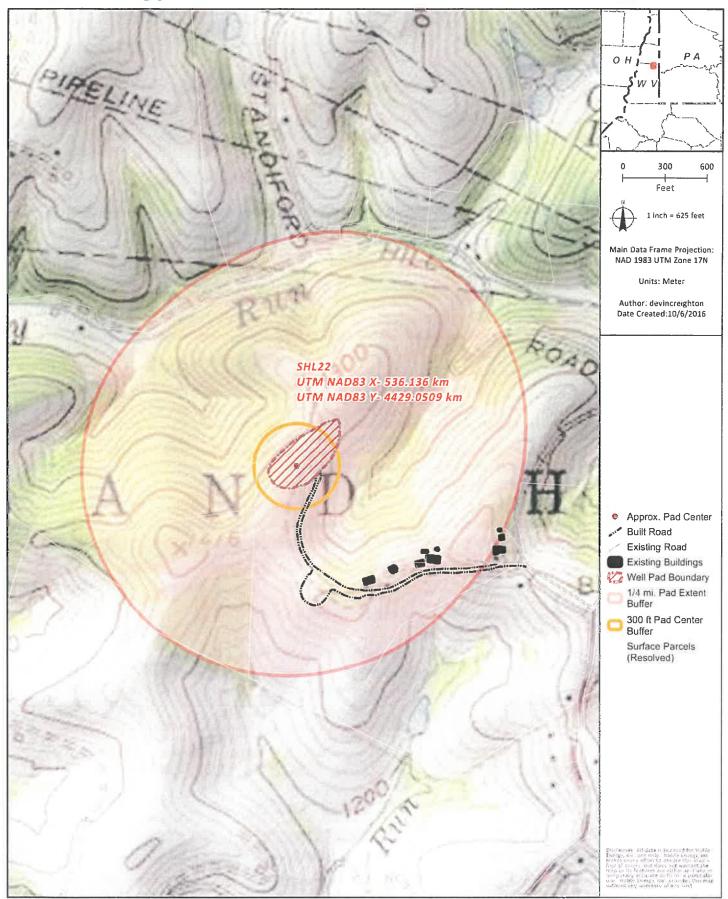
#### ATTACHMENT B

Area Map



# SHL22 Pad Marcellus Business Unit





#### **ATTACHMENT D**

**Regulatory Discussion** 

The following Federal and State air pollution control regulations will, or may apply to the SHL 22 Production Facility.

45CSR 2 Particulate Air Pollution from Combustion of Fuel in Indirect Heat Exchangers.

Noble Energy will be subject to the opacity requirements of this rule.

- 45CSR4 Objectionable Odors
- 45CSR6 To Prevent and Control Air Pollution from the Combustion of

The SHL 22 Facility will operate an enclosed combustion device and a flare.

45CSR13 Permits for Construction, Modification, Relocation, and Operation of Stationary Sources of Air Pollutants.

Noble Energy is required to submit a construction application.

45CSR16 Standards of Performance for New Stationary Sources Pursuant to 40CFR60.

The SHL 22 facility will have one engine subject to 40CFR60, Subpart JJJJ, 8 wells, one pneumatic diaphragm pump and storage tanks subject to 40CFR60, Subpart OOOOa.

45CSR22 Air Quality Management Fee Program

Noble Energy will pay a \$1,000 construction application fee, a \$1,000 NSPS fee and a \$200 Certificate To Operate fee.

40CFR60 Subpart JJJJ - Standards of performance for Spark Ignition Internal Combustion Engines.

Noble Energy will install one engine that is subject to this subpart.

40CFR60 Subpart OOOOa - Standards of performance for Crude Oil and
Natural Gas Facilities for which Construction, Modification or
Reconstruction Commenced After September 18, 2015

The SHL 22 facility will have equipment subject to 40CFR60, Subpart OOOOa.

Noble Energy, Inc SHL 22 Production Facility Permit G70-A Application

#### ATTACHMENT E

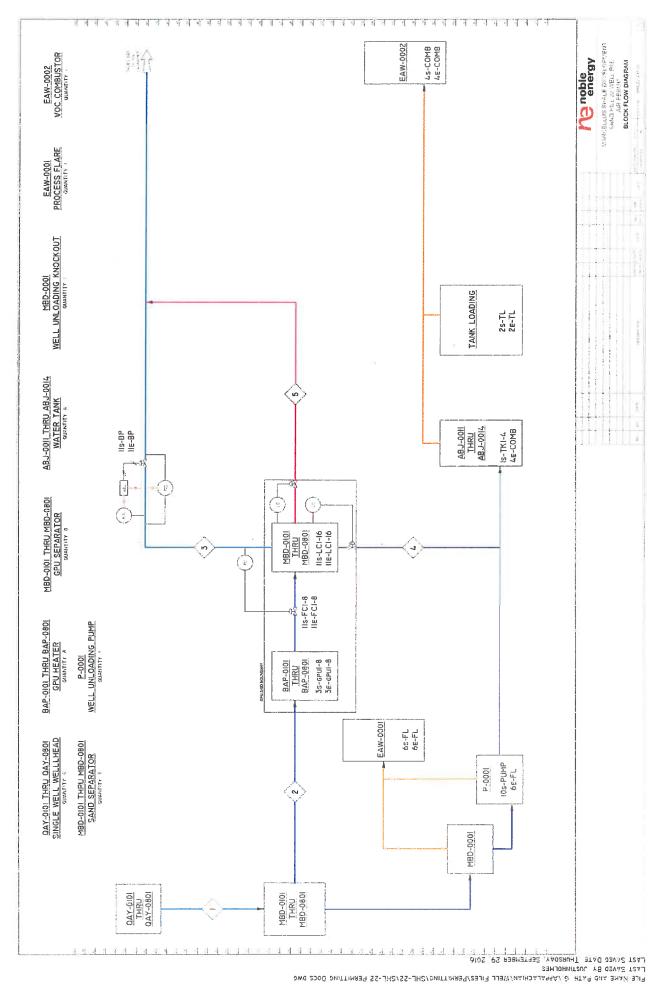
Plot Plan

S-PILOT	Emission Unit Description	400 BBL PRODUCED WATER TANK	WATER TANK UNLOADING EMISSIONS	2.0 MMBTU/HR HEATER	VAPOR COMBUSTOR - Leed Fab EC48	COMBUSTOR PILOT EMISSIONS	PROCESS FLARE - NOV	FLARE FILOT EMISSIONS	ARROW ENGINE COMPANY GAS GENERATOR	SANDPIPER G20 DIAPHRAGM PUMP	GPU FLOW VALVE CONTROLLER	BACKPRESSURE VALVE CONTROLLER	GPU LEVEL CONTROLLERS	EQUIPMENT COMPONENT FUGITIVES ESTIMATE										
S-PILOT 3S-GPU8 3S-GPU8 S-G	Emission Unit ID	1S-TK1	15-TK2	1S-TK3	1S-TK4	25-TL	3S-GPU1	3S-GPU2	3S-GPU3	3S-GPU4	3S-GPU5	3S-GPU6	35-GPU7	3S-GPU8	4S-COMB	33-PILOI	65-FL	/3-r/LOI	8S-FC 9S-GEN	105-PUMP	11S-FC1 THRU 8	11S-BP	11S-LC1 THRU 16	106
	LAUNCHER		\	4S-COMB & 5S-PILOT	STAD SE	S. GP172	3S-GPU6		7/2/1/		3S-GPUI	115+C3	VISERCE 118	1S-TK1 TO 1S-TK4	/IIS-FCI, IIS-LC									

Noble Energy, Inc SHL 22 Production Facility Permit G70-A Application

#### ATTACHMENT D

Process Flow Diagram



#### ATTACHMENT G

#### **Process Description**

The SHL 22 is an oil and natural gas production facility.

Condensate, gas, sand and water come from eight (8) natural gas wells through eight (8) sand separators.

Sand is routed to the Unloading Vessel which will also be used for well liquids unloading, controlled by flare [6C-FL]. Accumulated and will be removed periodically for proper disposal

Liquids from the Unloading Vessel will be transferred to the produced water tanks by Diaphragm Pump [10S-Pump] controlled by flare [6C-FL].

From the sand separators, the stream is routed to eight (8) Gas Production Units and Heaters [3S-GPU1-8] where fluid separation occurs, controlled by sixteen (16) Pneumatic Level Control Valves [11S-LC1-16].

Flow to the GPUs will be controlled by eight (eight) Pneumatic Flow Control Valves [11S-FC1-8].

Produced water from the separators flows into four (4) Water Tanks [1S-TK1-4] controlled by one (1) Vapor Combustor [4C-COMB].

Condensate and gas is routed from the GPUs directly to sales through one (1) Pneumatic Back Pressure Control Valve [115-BP].

Produced water will be trucked or pumped off location. Any loading emissions will be controlled by Vapor Combustor [4C-COMB].

If line power is not available, facility power will be generated by one (1) ARROW C-106 32, hp 4SRB engine [9S-GEN] or Acumentrics Remote Power System [8S-FC].

#### Source Aggregation Determination

Building, structure, facility, or installation are defined as all pollutant emitting activities which belong to the same industrial grouping, are located on one or more contiguous and adjacent properties, and are under common control.

The SHL 22 will operate under SIC code 1311. There are no other Noble Energy, Inc. facilities located on contiguous or adjacent properties to the site.

#### Attachment I **Emission Units Table**

(includes all emission units and air pollution control devices

Emission Unit ID <sup>1</sup>	Emission Point ID <sup>2</sup>	Emission Unit Description	Year Installed/ Modified	Desi	gn Capacity	Type <sup>3</sup> and Date of Change	Control Device <sup>1</sup>
IS-TK1-4	4E-COMB	400 bbl Produced Water Tanks	2016	400	bbl each	New	4C-COMB
2S-TL1	2E-TL1	Produced water truck loadout	2016	2044000	bbl/yr	New	4C-COMB
3S-GPUI	3E-GPU1	GPU Burner	2016	2.00	MMBtu/hr	New	NONE
3S-GPU2	3E-GPU2	GPU Burner	2016	2.00	MMBtu/hr	New	NONE
3S-GPU3	3E-GPU3	GPU Burner	2016	2.00	MMBtu/hr	New	NONE
3S-GPU4	3E-GPU4	GPU Burner	2016	2.00	MMBtu/hr	New	NONE
3S-GPU5	3E-GPU5	GPU Burner	2016	2.00	MMBtu/hr	New	NONE
3S-GPU6	3E-GPU6	GPU Burner	2016	2.00	MMBtu/br	New	NONE
3S-GPU7	3E-GPU7	GPU Burner	2016	2.00	MMBtu/hr	New	NONE
3S-GPU8	3E-GPU8	GPU Burner	2016	2.00	MMBtu/br	New	NONE
4S-COMB	4E-COMB	One (1) Vapor Combustor	2016	6000	scf/hr	New	NONE
5S-PILOT	5E-PILOT	One (1) Vapor Combustor Pilot	2016	12,5	scf/hr	New	NONE
6S-FL	6E-FL	flare	2016	74.727	MMBtu/hr	New	NONE
7S-PILOT	7E-PILOT	Flare Pilot	2016	0.264	MMBtu/hr	New	NONE
8S-FC	8E-FC	Fuel Cell	2016	1.44	gal propane/day	New	NONE
98-GEN	9E-GEN	ARROW C-106 Engine	2016	32	hp	New	NONE
10S-Pump	6E-FL	Sandpiper Diaphragm Pump	2016	20	sct/min	New	6C-FL
11S-FC1-8	11E-FC1-8	Pneumatic Flow Control Valves	2016	6.00	scf/hr	New	NONE
HS-BP	HE-BP	Pneumatic Back Pressure Control Valve	2016	6,00	scf/hr	New	NONE
11S-LC1-16	HE-LCI-16	Pneumatic Level Control Valves	2016	0.02	scf/hr	New	NONE

<sup>&</sup>lt;sup>1</sup> For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.

<sup>2</sup> For Emission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.

<sup>3</sup> New, modification, removal

<sup>4</sup> For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

### ATTACHMENT J

**Emissions Summary Sheets** 

EMISSION SUMMARY SHEET Noble Energy, Inc. SHL 22 Production Facility

Emisson Pont ID No. (Mast match Emisson Units Table & Piot Pion)	Erriysen Point	Emiss (Must mz	Emisser Uni Venied Thiough The Powi (Mict malch Emission Umin Table & Pot Pan)	Ar Poluron Conici Dewco (musi match Emisson Unis Table & Piol Plan)		Vent Time I Unit (chemic on	Verl Time for Emission Unit (chemical processes only)	All Brigurated Postulante - Chemical Name/CAS <sup>2</sup> (Specials VCCs & HAPS) See Detail Shoets	Maximur Unecottodo	Naxmum Pojenusi Uneontraciod Emissions <sup>2</sup>	Maximum Potentisi Cantrolost Eritisiums*		Emission Form or Phase (41 exit conditions, Solid Leyed or Gast/Vapor)	Est. Mehod Used <sup>®</sup>	Emission Concentration' (pom v or mg/m²)
		CA CA	Source	(D No	Device Type	Shari Torm*	Max (hr/yr)		1D:The	10ni/yr	15:fr	ay'vect			
26-71.2	Vent	25-TL1	Produced water truck loadout	N/A	N/A	N/A	N/A	VOC	0.53	2.30	0.53	2.30	2.30 Gas/Vapor	AP-42	
								HAPs	0.00	0.48	0.00	0.48	0.48 Gas/Vapor	AP-42	
								NOX	0,17	0.73	0.17	0.73	0.73 баз/Уарог	AP-42	
				1		*		9 9	0.14	0.61	0.14	0.61	0.61 Gas/Vapor	AP-42	
3€ GPU1	Heater Stack	35-GPU1	GPU Hurner	4/2	A/N	N/A	A/S	203	10.0	0.04	10.0	0.04	O.O. C. Arrapor	AP-42	
								502	0.00	0.00	00.00	0000	O.DC Gas/Vapor	AP-42	
								Formuldshods	100	0.00	1000		O.Do Particulate	AP-42	
								HAPs	8 8	0.00	000	000	Gas/Vapor	VP-42	
								CO2e	200.10	876.42	200.10		876.42 Gas/Vapor	AP-42	
								NOX	0.17	0.73	0.17		0.73 Gas/Vappr	AP-42	
								CO	0.14	0.61	0.14		0.61 Gas/Vapor	AP-42	
3E-GPUZ	Heater Stack 35-GPU2	35-GPU2	GPU Burner	N/A	N/A	N/A	N/A	voc	0.01	0.04	0.01		1	AP-42	
								502	0.00	00:0	00'0		1	AP-42	
								PIM10	10.01	90.0	0.01		0.06 Particulate	AP-42	
								Formaldehyde	0.00	0.00	0.00		0.00 Gas/Vapor	AP-42	
								HAPs	0.0	0.01	0.00		0.01 Gas/Vapor	AP-42	
								CO2e	200.10	876.42	200.10	1	876.42 Gas/Vapor	AP-42	
								NOx	0.17	0.73	0.17		0.73 Gas/Vapor	AP-42	
								CO	0.14	0.61	0.14		0.61 Gas/Vapor	AP-42	
3E-GPU3	Heater Stack	35-GPU3	GPU Burner	N/A	N/A	N/A	R/A	VOC	0.01	0.04	0.01		-	AP-42	
								202	0.00	0.00	0.00		- (	AP-42	
								PM10	0.01	90.0	0.01		0.06 Particulate	AP-42	
								roi maidenyde	3 5	200	00.0		0.00 Gas/Vapor	AP-42	
								CO2e	200.10	876.42	200.10	18	876.42 Gas/Vapor	AP-42	
								2407	21.0	0.73	210		0.72 (52/1/2007	Ab. 43	
			-					S S	0.14	0.61	0.14		0.61 Gas/Vapor	AP-42	
36.60114	Heater Stack	35.50114	SPI Burner	N/A	N/A	N/A	N/A	VOC	0.01	0.04	0.01		0.04 Gas/Vapor	AP-42	
10.00.00	mentel state			L dec		Į.		502	0.00	0,00	0.00		0.00 Gas/Vapor	AP-42	
								PM10	0.01	0.00	0.01		0.05 Particulate	AP-42	
								Formaldehyde	0.00	00'0	0.00		0.00 Gas/Vapor	AP-42	
								HAPs	0.00	0.01	0.00		0.01 Gas/Vapor	AP-42	
								coze	200,10	876.42	200.10		876.42 Gas/Vapor	AP-42	
								NOx	0.17	E2.0	0.17		Gas/Vapor	AP-42	
								8	0.14	0.61	0.14		0.61 Gas/Vapor	AP-42	
3E-6PU5	Heater Stack	35-GPUS	GPU Burner	N/A	N/A	N/A	N/A	VOC	0.01	0.04	0.01		0.04 Gas/Vapor	AP-42	
								203	0.00	0.00	0.00		0.00 Gas/Vapor	AP-42	
								PM10	0.01	0.06	0.01		0.06 Particulate	AP-42	
								Formaldehyde	00:00	00.00	00:00		0.00 Gas/Vapor	AP-42	
								HAPs	0.00	0.01	0.00		0.01 Gas/Vapor	AP-42	
								C02e	200.10	876.42	200.10		876.42 Gas/Vapor	AP-42	
								NOX	0.17	0.73	0.17		0.73 Gas/Vapor	AP-42	
								5	0.14	0.61	0.14		0.61 Gas/Vapor	AP-47	
2000	The second second		200	W/V	27.00	47/4	Q/N	202	100	0.04	000		0.04 Gas/Vannr	4P-47	
at-urue	neater Mack	33-0700		e Ju	£ /£			502	000	000	00.0		0.00 Gas/Vapor	AP-42	
								PM10	100	0.06	10.0		0.06 Particulate	AP.42	
								Formaldehyde	000	00.0	0.00		0.00 Gas/Vapor	AP-42	
								HAPs	0.0	0.01	0.00		Gas/Vapor	AP-42	
								COZe	203,10	876.42	200,10	1	876.42 Gas/Vapor	AP-42	
												ı			

EMISSION SUMMARY SHEET Noble Energy, Inc. SHL 22 Production Facility

Emisson Concentration (ppmv or mpint)																							FESCO Study / Tanks	FESCO Study / Tanks																												
			Т	П	Т	Т	Ţ	30r AP-42	Т	Т	Т	Τ	Τ.	Г	Г		Г	Г	Π	por AP-42	ate	par AP-42	П	7		00r AP-42		П		Т		DOI AP-42	1	Т	Г	Т	Т	ı	Г		Г	Γ	Γ	Γ	Г	Γ		ate AP-42	Г			
Enissuca Form or Phase (Al unit cendions, Sold, Liquid or Gas/Vaport		0.73 Gas/Vapor	0.61 Gas/Vapor	0.04 Gas/Vapor	0.00 Gas/Vapor	0.06 Particulate	0.00 Gas/Vapor	0.01 Gas/Vapor	0.42 Gas/vapar	0.63 Gas/Vapor	O Od Gas/Vapor	0.00 Gas/vapp	0.06 Particulate	0.00 Gas/Vapor	0.01 Gas/Vapor	876.42 Gas/Vapor	3.48 Gas/Vapor	18.96 Gas/Vapor	Gas/Vapo	0.05 Gas/Vapor	Particulate	09 Gas/Vapor	0.51 Gas/Vapor	0.04 Gas/Vapor	0.11 Gas/Vapor	0.02 Gas/Vapor	0.01 Gas/Vapor	0.00 Gas/Vapor	0.00 Gas/Vapor	0.00 Particulate	SS Cas/val	3 35 Garlyanor	0.25 Gas/Vanor	02 Gas/Vanor	0.02 Gas/Vanor	0 10 Gac/Vanor	0.03 Gas/Vapor	0.00 Gas/Vapor	31.42 Gas/Vapor	0.09 Gas/Vapor	0.08 Gas/Vapor	0.01 Gas/Vapor	74 Gas/Vapor	0.00 Gas/Vapor	9.00 Gas/Vapor		0.00 Gas/Vapor	0.00 Particulate	3 30 00-01			
Masımum Potontial Controlled Emissions	Handyr							6	à								L		Ľ		76.7	1 6029.09												160									=									
Макиты	ib/hr	0.17	0.14	0.01	0.00	0.01	0.00	0.00	01.002	0.14	100	0.00	0.01	00:00	0.00	200.10	0.80	4.33	í	0.01	}	1376.51	0.12	0.01	0.02	0.03	00:00	00.00	0.00	0.00	7.	18 18	1 33	366.22	0.00	000	0.16	0.01	7,17	0.02	0.02	0.00	25.97	00:0	0.0	00.0	0.00	0.00	37.0			
Maxmum Polential Uncoviroid Emissions	lon'yr	0.73	0.61	0.04	0.00	0.06	8 8	0.01	0.73	0.61	0.04	000	0.06	0.00	0.01	876.42	3.48	18.96		0.05	:	6029.09	25.44	00:0	5.37	1.13	0.01	0.00	000	000	6.03	167.78	12.27	1604.02	0.02	01.0	1.44	0.11	31.42	60'0	0.08	0.01	113.74	0.00	0.00	0,00	0.00	0.00	2 30			
Maximum Uncontroles	lb(fa	0.17	0.14	0.01	000	0.01	0.00	0.00	0.170	0.14	100	000	10.0	0.00	0.00	200.10	08.0	4.33	1	0.01	î	1376.51	5.81	0.00	1.23	0.26	0.00	0.00	0.00	0.00	17.0	016.82	66.69	366.22	0.00	0.02	7,87	0.58	71.17	0.02	0.02	0.00	25.97	0.00	00'0	0,00	0.00	00'0	27.00			
All Regustred Pokulone - Chemical Name/CAS* (Specate VOCs & HAPS) See Detall Shasts		NON	8	VOC	202	PMIO	Formaldehyde	HAPS CO2a	2002	00	200	502	PM10	Formaldehyde	HAPs	CO2e	NOK	8	VOC	502	PM10	203	VOC	HAPs	VOC	HAPS	NOx	CO	VOC	PMID	NOR	200	HAPe	C02	NOX	2	VOC	HAPs	CO2	NOx	00	voc	CO2	NOx	8	voc	502	Pt/410	2000			
	Max (hr/yr)			A/N						-1	N/A						Ī	-	N/A				N/A	П	N/A	1			N/A			N/A			Ī		N/A					N/A				N/A						
Ven Time for Emission Unil (chemes if processes	Short Term <sup>é</sup>		-	V/N							N/A								N/A				N/A		N/A				N/A			11/4					N/A					N/A				N/A			_			
naro! Devke nrason Unte o! Pian)	Dovice Type			N/A										N/N								N/A				ECD		ECD.				A/N			V/N	ı,				flare					N/A				N/A			
Air Polision Curitol Device (mel misch Einescon Unte Table & Plot Plan)	ID No			N/A							N/A								N/A				4C-COMB		4C-COMB				N/A			N/A					6C-FL					M/A				N/A						
Emesson Umi Ventod Through This Point (Must match Emesson Units Tobls & Ptot Pton)	Source		:	GPU Burner							SPtJ Burner								One (1) Vapor Combustor				One (1) Vapor Combustor		One (1) Vapor Cambustor				One (1) Vapor Combustor Pilot			200					Sandolper Diaghtagm Pump					Flare Prior				Fuel Cell						
Embs (Must m	ID No			35-GPU7							35-GPU8								45-COMB				1S-TK1-4		25-Tt.1				55-PILOT			66.59	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1				105-Pump	1				75-PILOT				85-FC						
Тура				Heater Stack							Heater Stark								Slack				Stack		Stack				Stack			9000	-				Stack					Stack				Stack						
Emizzari Pont ID No (Must match Emission) (Insis Tabes & Port Pan)				3E-GPU7	ofe 3 in	, <u>u</u> ,					3F-GPUR								46 -CDMB				4E-COMB S		4E-COMB S				SE-PILOT S			5 13-19					9					76-PILOT				8E-FC						

EMISSION SUMMARY SHEET Noble Energy, Inc. SHL 22 Production Facility

Emisson Point ID No   Must mister Emisson   Unis Table & Plot Pent)	Етцануя Роли Туре <sup>*</sup>		Emissen Una Vented Through Tha Penti (Kusi maleh Emisson Unit. Tabra & Pol Plen)	Avr Poviston Control Device (must match Emissen Units Täble & Plot Pan)		Von Time for Emissbir Uni (chemisal processors)		All Rogululed Pollutants - Chemical NamolCAS <sup>2</sup> (Specials VOCe & HAPS) See Detail Swedis	Мамтыт Рофаны Илсоектовей Етизакия <sup>3</sup>	Polenta: Émissiono <sup>3</sup>	Masmum Potential Controlled Emissions		Etnesson Form or Phase (Al exit conditions, Solid, Liqued or Gaes/Vaport	Est Melhod Used?	Emission Concantization <sup>†</sup> (ppmv út mg/m <sup>†</sup> )
		oM CI	Source	NO No.	Device Type	Short Ma	Max (ht/yt)		th.fhr	ton/yr	th:fhr	sordyr			
							ž	×CN	0.99	4.33	0.20	0.87 Ga	0.87 Gas/Vapor	Manufacturer	
							8	0	0.81	3.55	0.34	1.4B Ga	1.48 Gas/Vapor M	Manufacturer	
9E-GEN	Engine Stack 95-GEN	98-GEN	ARROW C-106 Engine	9C-GEN CAT	NSCH	N/A	N/A VC	voc	N/A	N/A	N/A N	N/A Ga	Gas/Vapor N	Manufacturer	
					_		×	202	0.00	00'0	00'0	0.00 Ga	0.00 Gas/Vapor Al	AP-42	
							ä	PEALO	0.03	0.01	00.0	0.01 Pa		AP-42	
					_		3	Formaldehyde	0.01	0.03	0.01	0.03 Ga	0.03 Gas/Vapor A	AP-42	
							Ĩ	HAPs	0.01	0.03	10.0	0.03 Ga	0.03 Gas/Vapor A	AP-42	
							ŭ	CO2e	38.34	167.91	38,34	167.91 Gas/Vapor		AP-42	
112-FC1-8	Vent	115-FC1-8	Pneumatic Flow Control Valves	N/A	N/A	N/P.	N/A VC	VOC	2.46	10.76	2.46	10.76 Gas/Vapor		HYSYS	
							Î	HAPs	0.20	0.86	0.20	0.85 Ga	0.86 Gas/Vapor H	HYSYS	
							ŭ	CO2e	331.25	1450.88	331.25	1450.88 Gas/Vapor		HYSYS	
11E-8P	Vent	11S-BP	Pneumain Back Pressure Control Valve	N/A	N/A	N/A	N/A VC	voc	0.31	1.34	0.31	1.34 Ga	1.34 Gas/Vapor H	SASAH	
							Î	HAPs	0.02	0.11	0.02	0.11 Ga	0.11 Gas/Vapor H	SASAH	
							ŭ	CO2e	41.41	181.36	41.41	181.36 Gas/Vapor	Г	SASAH	
116-101-16	Vent	115-171-16	Pneumatic Level Control Valves	14/4	N/A	N/A	N/A VC	VOC	10.0	0.06	0.01	0.06 Ga	0.06 Gas/Vapor	HYSYS	
	-2-						ī	HAPs	0.20	00.00	0.20	0.00 Ga	0.00 Gas/Vapor H	HYSYS	
					_	_	۲	600	184	8.06	1 84	8 DE G3	8 DE GacWanar	VAVA7	

# Attachment K FUGITIVE EMISSIONS DATA SUMMARY SHEET

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted

for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS	į
1.) Will there be haul road activities?	
☐Yes ②No	
If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.	
2.) Will there be Storage Piles?	
☐ Yes	
If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET.	
3.) Will there be Liquid Loading/Unloading Operations?	
☑ Yes   □Yo	
If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.	
4.) Will there be emissions of air pollutants from Wastewater Treatment Evaporation?	
☐ Yes   ☑ Yo	
5.) Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, op ended valves, sampling connections, flanges, agitators, cooling towers, etc.)?	en-
☑Yes ☐No	
If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.	
6.) Will there be General Clean-up VOC Operations?	
☐ Yes ☑No	
If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.	
7.) Will there be any other activities that generate fugitive emissions?	
☐ Yes ☑ Yu	
If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.	

If you answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions Summary."

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants Chemical Name/CAS <sup>1</sup>	Maximum Uncontrolled Potential Emissions <sup>2</sup>		Maximum Potential Controlled Emissions		Est. Method Used
		lb/hr	ton/yr	lb/hr	ton/yr	
Haul Road/Road Dust Emissions Paved Haul Roads						
Unpaved Haul Roads						
Storage Pile Emissions						
	VOCs	1.75	7.67	0.53	2.30	EE / EPA
Loading/Unloading Operations	HAPs	0.00	1.61	0.00	0.48	EE / EPA
Wastewater Treatment Evaporation & Operations						
Equipment Leaks	VOCs	Does not apply	7.72	Does not apply	7.72	EE/EPA
Equipment Leans	HAPs	Does not apply	0.51	Does not apply	0.51	EE/EPA
General Clean-up VOC Emissions						
Other						

List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, Ct

VOCs, H<sub>2</sub>S, Inorganics, Lead, Organics, O<sub>3</sub>, NO, NO<sub>2</sub>, SO<sub>2</sub>, SO<sub>3</sub>, all applicable Greenhouse Gases (including CO<sub>2</sub> and methane), etc. DO NOT LIST H<sub>2</sub>, H<sub>2</sub> O<sub>2</sub>, and Noble Gases.

<sup>&</sup>lt;sup>3</sup> Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

<sup>&</sup>lt;sup>o</sup> Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

LEAK SOURCE DATA SHEET (Please see attached fugitive emissions spreadsheet)

Source Category	Pollutant	Number of Source Components <sup>1</sup>	Number of Components Monitored by Frequency <sup>2</sup>	Average Time to Repair (days)³	Estimated Annual Emission Rate (lb/yr)
Pumps <sup>5</sup>	light liquid VOC <sup>6,7</sup>		Bi-annually	15	251
	heavy liquid VOC®				
	Non-VOC <sup>9</sup>				
Valves <sup>10</sup>	Gas VOC	06	Bi-annually	15	1251
	Light Liquid VOC	64	Bi-annually	15	3090
	Heavy Liquid VOC				
	Non-VOC				
Safety Relief Valves <sup>11</sup>	Gas VOC	16	Bi-annually	15	49
	Non VOC				
Open-ended Lines 12	VOC	8	Bi-annually	15	49
	Non-VOC				
Sampling Connections <sup>13</sup>	VOC				
Connectors	Non-VOC				
Compressors	voc				
	Nan-VOC				
Flanges	voc	148	Bi-annually	15	159
	Non-VOC				
Other	VOC	88	Bi-annually	15	9382
	Non-VOC				

3.13 See notes on the following page.

SHL 22 Production Facility Equipt Component Fugitives Estimate FUG

	Counts	Emission Fuctor <sup>2</sup>	% Control Efficiency % VOC	% VOC	VOC Emissions	issions	Benzene	Toluene	E-benzene	Xylene	n-Hexane	224-TMP	%CH4	CH4 Emissions	issions	00.
		lb/ln/eoinpon ent			lb/hr	tpy	lb/yr	lb/yr	lbíyr	lb/yr	lb/yr	lb/yr		lb/hr	ids	tpy
Valve																
Gas/Vapor	06	0.00992	э	16	0.14	0.63	0.18	0.38	0.04	0.61	13.06	0.00	59.83	0.53	2.34	49.13
Light Liquid	10	0.00551	0	100	0.35	1.54	3.55	19.00	4.63	35.68	235.08	24.71	1.17	0.00	0.05	0.38
Water/Oil	150	0.000216	0	50	10.0	0.03	0.14	0.74	0.18	1.40	0,92	0.00	1.17	0.00	0.00	10.0
Pumps Seals																
Light Liquid	_	0.02866	c	100	0.03	0.13	0.29	1.54	0.38	2.90	19.11	2.01	1.17	00.0	00'0	0.03
Water'Oil	_	0.0000529	÷	30	0.00	00.0	0.00	0.00	0.00	10.0	0.04	000	1.17	00.0	00'0	0.00
Flanges																
Gas Vapor	99	0,00086	¢	91	10.0	0.04	0.01	0.02	0.00	0.04	0.75	0.00	59.83	0.03	0.14	13
Light Liquid	7	0.000243	0	100	10.0	0.04	01.0	0.52	0.13	86'0	6.48	89.0	8	10.0	0.04	08.0
Water Oil	SF	0.000000617		05	0.00	00'0	0.00	0.02	0.00	0.03	0.02	00'0	100	0.00	00.0	0.03
Open-Ended Lines																
Gas-Vapor	30	0.00441	٥	9	10.0	0.03	0.01	0.02	00.0	0.02	0.52	00'0	59.83	0.02	60'0	1.94
Light Liquid	=	0.00309	=	100	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	901	0.00	0.00	0.00
Water/Oil	*	0.008)6	٥	20	0.00	0.00	0.00	0.00	00'0	0.00	0.00	0.00	901	0.00	000	0.00
Other																
Gas:Vapor	FI	60.0194	=	91	0.07	0.33	0.09	0.20	0.02	0.32	6.81	0.00	59.83	0.28	1,22	25.62
Light Liquid1	200	0.0165	=	100	0.13	95.0	1.33	7.11	1.73	13.36	88.00	9.25	100	0.13	0.58	12.14
Water/Oil	99	0.0309	0	90	0.87	3.79	17.43	93,22	22.74	175.08	115.35	0.00	100	1.73	7.58	159.16
Connectors																
Gas/Vapor	425	0,000441	0	91	0.03	0.13	0.04	80.0	0.01	0.13	2.74	0.00	59.83	0.11	0.49	10.31
Light Liquid	200	0.000463	0	100	60.0	0.41	0.93	4.99	1.22	9.37	61.73	6.49	001	60.0	0,41	8.52
WaterOil	112	0.000243	O	50	0.01	0.06	0.27	1.47	0.36	2.75	1.81	0.00	100	0.03	0.12	2.50
	Total	Fotal Emissions			1.75	7.72	24.11	127.85	31.09	239.92	550.61	43.14		2.95	12.91	271.02

# Attachment L EMISSIONS UNIT DATA SHEET STORAGE TANKS

Provide the following information for each new or modified bulk fiquid storage tank

I. GENERAL INFORMATION (required)						
1 Bulk Storage Area Name		2. Tank Name				
SHL 22 Produced Water Tank Battery		490 551 1	Produced Water Tanks			
3 - Emission Unit ID number		4 Emission Point ID number				
1S-TK1-4	1E-TK1-4					
5. Date installed or Modified tror current toules.  6. Type of change:						
		New Construction New Stored Mat	erral Other			
7A. Description of Tank Modification (4) applicable)						
2B. Will more than one material be stored in this tank? If so, a separate form mus	a be completed for each me	atorial.				
Yes No						
7C. Provide any limitations on source operation affecting emissions. (production of	rariation, etc.)					
L TANK INFORMATION (required)						
<ol> <li>Design Capacity ispecify harrels or gallows. Use the internal cross-sectional i</li> </ol>		-				
	400 bi					
9A. Tank Internal Diameter (ft.)	12	9B. Tank Internal Height (A.)		20		
10A. Maximum Liquid Height (h.)	19.5	10B. Average Liquid Height (fl.)		10		
HA. Maximum Vapor Space Height (ft.)	18.3	11B, Average Vapor Space Height (ft.)	393 661	10		
<ol> <li>Nominal Capacity (specify barrels or gallous). This is also known as "workir</li> <li>Maximum annual throughput (gallyt) per lank</li> </ol>	21,462,000	13B. Maximum daily throughput (gal-day) p		58,800		
	1278 per tank	15. Maximum tank fill rate (gal/inm)	тт ынк	1171.8		
	Bottom Loading	to the time is the interest		1171.0		
17. Is the tank system a variable vapor space system?	-					
If yes, (A) What is the volume expansion capacity of the system (gal)?						
(B) What are the number of transfers into the system per year?						
18. Type of tank (check all that apply):						
Fixed Roof X vertical horizontal flat roof X cor	se roofdome roof	other (describe)				
External Floating Roof pontion roof double deek roof	WALLES .					
Domed External (or Covered) Floating Roof						
Internal Floating Roof						
Variable Vapor Space litter root diaphragm						
Pressurizedsphericalcylindrical						
Underground						
Other (Describe)						
SECTION III (required if did not provide TANKS Summary Sheets)						
TANK CONSTRUCTION AND OPERATION INFORMATION						
19 Tank Shell Construction:						
	r (describe)		welded			
20A Shell Color green	20B. Roof Color	green	200 Year Last Painted:	new		
21. Shell Condition (if metal and unbred)  Riveted Light Rust Dense Rust Phot Applicable						
	228 If ics, operating temp		220 Hazas, how is heat provided to tar	1.1		
22A. Is the tank heated? Yes Tho		erstone.		· k *		
23. Operating Pressure Range (psig):	thá	-0.025 - 1	na			
24. Is the tank a Vertical Fixed Roof Tank?	24A Harry for dome root		24B If yes, for come root, provide slop	tit ne		
☑Yes ☐No	200 COLUMN STREET FOR	Interior status (10)	0.00			
			12.0			
25 Complete them 25 for Floating Roof Funks  25A Year internal Floaters Installed						
25H. Primary Scal Type (check ours)						
Metallic (mechanical)  Vapor mounted resilient seaf	Liquid mounted res	silient seaf				
25C Is the Floating Reof equipped with a secondary stall Yes	□Nc					
, , , , , , , , , , , , , , , , , , , ,						
28D If yes, how is the secondary sent mounted? (Glock one) Shoe	Rim					
250 Is the floating roof equipped with a weather shield. Yes [ Yes ]	No					
25F Describe deck fittings.						

26. Complete the following	section for Internal	Floating Roof Tanks		Does not apply					
364 Fleet Time		Velded		76H Fer holied decks, provide deck construction					
26C Deck seam. Continu	ous sheat construction:			l					
S ft wide	∐6 ft wide ☐7	7 ft wide5 x 7.5			er (describe)				
26D. Deck seam length (ft.)	26F Area of Jeck (I	) <sup>2</sup> }	26F For colsons	apported tanks, # of columns		25G For column sap	ported tanks, dometer	of column:	
SITE INFORMATION:	1		1						
23. Provide the city and sta	ite on which the data in	this section are based:			Pi	ishurgh, Pennsylvania			
28. Daily Avg. Ambiem To		a total in the contract				50.31			
29. Aumal Avg. Maximan						59.88			
30. Annual Avg. Minomon						40.73			
31. Avg. Wind Speed (nap)						9.08			
32. Annual Avg. Solar Inc.		-day)				1202.96			
33. Atmospheric Pressure						14.11			
LIQUID INFORMATIO	N:								
34. Avg. daily temperature	range of balk liquid (*	F);							
34A, Minimum (°F):				10,02	34B. Masimum (°F);				59.K8
35. As g. operating pressur	e range of tank (psig):								
35A. Manmon (psig):				0,09	35B. Maximum (psig):				1.15
36A. Minimum liquid surf	ace tenuneraliste (°F):				36B. Corresponding vapo	e pressure (usia):			2.39
37A. Avg. liquid surface to					37B. Corresponding vapo				3.01
38A. Maximum liquid surf					38B. Corresponding vapo				
					Sair. Corresponding vapo	Diesene (Issu)			3.75
39. Provide the following (		the stored in the ting	Add additional page	1		1		1	
39A. Material name and co	miposition.			Produce	u Water				
39B. CAS number:						1		ļ	
39C. Liquid density (lb/ga				5.					
39D. Liquid molecular wei	ght (lb.lb-mole):			9.	2				
39E. Vapor molecular wei	ghi (lb-lb-mole):			64	9				
39F. Maximum true vapor	pressura (psia);			3,3	15				
39G Maxim Reid vapor p	ressure (psia).			6					
39H. Mondo Storage per y	un .								
	From:			la:	to .	1			
	To:			De	re.				
VI. EMISSIONS AN	D COSTROL D	FVICE DATA (re	ouired)						
40. Emission Control De			· quireur						
Does Not Apply		2	Rupture Disc (	osial					
Carbon Adsorption 1		Yi	Inert Gas Blank						
Vent to Vapor Combu	stran Davine 1 (una	as sampustosa Ha-an							
Condenser 1	iscon beace 1 (vap	or compusions, nares	Conservation V						
I _			Conservation 4	ziir (bash)					
lOther I (describe) - \	Japor Recovery Unit		F3						
			Emergency Rel	iel Valve (psig)					
Complete appropriate A	tic Pollution Control	Device Sheet							
41 Expected Emission I		ata or Calculations be	re or elsewhere in	the application).					
Material Name and	Flashing Loss		Breathing Loss		Working Loss		Total uncont. Emi	ssions Luss	Estimation
Cas No.	Uncontrolled	1.	Uncontrolled	I	Uncontrolled	L.		l	Method <sup>1</sup>
	lb/hr	tpy	lh/hr	Тру	lb/hr	tpy	tb/hr	103	
Total uncontrolled VOC emissions for all tanks	4.31	18.87	0.56	2,46	0.94	4.11	5.8t	25,44	PPA, SS
		<del> </del>							
		<del>                                     </del>	-						
		<del> </del>						-	
		<del> </del>							
	<u> </u>	-				-			1
		ļ							
		ļ							ļ
									(

IPA PPA Lansson Factor MB Material Balance SS Similar Source ST Similar Source Test. Throughput Data, O Other (specific)
Remember for attach gantisa in each distance social one of FENA's Similar Society and other model ling Source is supply with

## TANK TRUCK LOADING EMISSION UNIT DATA SHEET

Furnish the fullowing information for each new or modified bulk liquid transfer area or landing rack at the natural gas production pail. This toria is to be used for bulk liquid transfer diseastions to tank tris ki

Identification Number (Emission Unit ID from Equipment List):			2S-TL1	Emission	Point ID:	2E-TL1	4E-COMB	
2. Type of cargo vessels  Droms	s accomodated at this rack or transfer poin	t (eheek as many a e Vessels	s apply):	□Rai! Tank Cars		Tank Trucks		
3. Loading Area Data:								
Number of pumps:				E				
Number of liquids load	Number of liquids loaded			i				
Maximum number of t	ank trucks loading at one time.			1				
4. Does bailasting of mi	arine vessels occur at this londing area?  Does not apply							
5. Describe cleaning loc N/A								
6. Are tank trucks pressure tested for leaks at this or any other location?  TYES, describe:								
7. Projected Maximum	Operating Schedule (for rack or transfer p	oint as a wholer						
Maximum	Jan Mar.	Apr June		July - Sept.	Oct Dec.			
bours day	24	24		24	24			
days/week	7	7		7	7			
8. Bulk Liquid Data tad	ld pages as necessary)							
Pump ID No.	TBD							
Liquid Name	Produced Water							
Max, daily throughput (1000 gal day)	235,2							
Max, annual throughput (1000 gal-yr)	R5.848							
Londing Method	SUB							
Max Fill Rate (gal min)	TBD							
Average Fdl Time (min leading)	TBD							
Max Hillk Liquid Temperature (°F)	59,9							
True Vapor Pressure	Pressure 3.75							
Cargo Vessel Condition	TBD							
Control Equipment or Medical <sup>3</sup>	TO - 4C-COMB							
Minimum collection officiency (%a)	7()% <sub>a</sub>							
Manager courst efficiency (*5)	3846							
T. Control of the Con			4 (*					

Maximum Emission	Loading (thitir)	1.75	nacontrulled			
Kate	Annual (ton/yr)	7.67	uncontrolled			
Estimation Method *		E	PA			
Notes:						
<sup>4</sup> BF Bomm Fill S2	Splash Fill SUB	Submerged Fill	·			
<sup>2</sup> At maximum baik liquid t	At maximum baik liquid temperature					
B. Ballasted Vessel, C.	Cleaned, Uncleane	d (dedicated service).	O other (describe)			
4 List as many as apply (cor	uplete and salmit appro	priate Air Pollution	Control Device Sheet	as Attachment "H"),		
CA = Carbon Adsorption						
VB Dedicated Vapor Bul.	ance (closed system)					
ECD = Enclosed Combuse	ion Device					
F = Flare						
TO - Thermal Oxidation or	Incineration					
* EPA   EPA Emission Fac	etor as stated in AP-42					
MB = Material Balance					· · · · · · · · · · · · · · · · · · ·	
TM Test Measurement	based upon test data sub	enutal				
D other (describe)					·····	
						a the state of the
9. Proposed Monitoria	g, Recordkeeping, F	eporting, and Te	gaits			
Please propose monitor	ing, recordkeeping, a	nd reporting as orde	er to demonstrate co	mpliance with the propose emissions lin		in order to demonstrate compliance with the proposed
MONITORING					RECORDKEEPING	
	Ten	k Luading Through	lament.		Maintain loss	ling throughput records.
	1100	K Edwiding (through	infrat		(Maritan Post	ing moughput rections.
REPORTING					TESTING	
		Upon Request				NA
İ						
AMONITORING Please is a and describe the process parameters and ranges that are proposed to be monitored in index to demonstrate compliance with the operation at this process equipment operations are pollution control device.						
RECORDKEEPING Please describe the proposed recordlecening that will secondary the monutaring						
REPORTING Please desc	UPORTING Please describe the proposed it equation of reporting of the recordiograph					
FESTING. Pleases deverbe any proposed convisions testing for the process equipment are pollution control devies						

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty

# NATURAL GAS FIRED FUEL BURNING UNITS EMISSION DATA SHEET

Complete the information on this data for each Gas Producing Unitis). Heater Treaterts), and in-line heaterts) at the production pad. Reboiler information should be entered on the Glycol Dehydration Emission Unit Data Sheet.

	_		_	_	_		_	_
Fuel Heating Value (Btu/scf)"	1200	1200	1200	1200	1200	1200	1200	1200
Design Heat Input. (mmBtuthr) <sup>5</sup>	2.0	2.0	2.0	2.0	2,0	2.0	2.0	2.0
Control Device <sup>4</sup>	None							
Type <sup>2</sup> and Date of Change	New							
Year Installed Modified	- 2017	2017	2017	2017	2017	2017	2017	2017
Emission Unit Description (Manufacturer / Model #)	Heater							
Emission Point 1D#²	3E-GPUI	3E-GPU2	3E-GPU3	3E-GPU4	3E-GPU5	3E-GPU6	3E-GPU7	3E-GPU8
Emission Unit ID #	3S-GPUI	3S-GPU2	3S-GPU3	3S-GPU4	3S-GPUS	3S-GPU6	3S-GPU7	3S-GPU8

Enter the appropriate Emission Unit (or Sources) identification numbers for each finel burning unit located at the production pad. Gas Producing Unit Burners should be designated GPU-1, GPU-2, etc. Heater Treaters should be designated HT-1, HT-2, etc. For sources, use 15, 28, 35...or other appropriate designation. Enter glycol dehydration unit Reboiler Vent data on the Glycol Dehydration Unit Data Sheet.

Factor the appropriate Emission Point identification numbers for each fact borning unit located at the production pad. Gas Producing Unit. Burners should be designated GPU-1, GPU-2, etc. Heaters bound be designated HT-1, HT-2, etc. For emission points, use LE, 2E, 3E...or other appropriate designation.

New, medification, removal

Complete appropriate air pullution control device sheet for any control device.

Teater design heat input capacity in mmBluthr.

Enter the fuel hearing value in Buystandard cubic foot.

#### NATURAL GAS COMPRESSOR/GENERATOR ENGINE DATA SHEET

Source Identification Number		9S-4	GEN				
Engine Ma	nufacturer and Model	ARRO	W C-106				
Manufacturer's Rated bhp/rpm		32 (6	y 800				
So	narce Status2	7	٧S				
Date Installe	d/Modified/Removed3	2/1/	2017				
Engine Manufact	ured/Reconstruction Date4	T	BD				
	tationary Spark Ignition Engine Subpart JJJJ? (Yes or No) <sup>5</sup>	NO					
Engine. Fuel and	Engine Type <sup>6</sup>	RI	34S				_
Combustion	APCD Type <sup>₹</sup>	A/F	NSCR.				
Data	Fuel Type <sup>5</sup>	R	kG.				
-	H <sub>2</sub> S (gr/100 sef)	≤0.2					
	Operating bhp/rpm	_	32 <i>(y</i> 800			· ·	
	BSFC (Btu/bhp-hr)	10350					
	Fuel throughput (ft <sup>3</sup> /hr)	12780					
	Fuel throughput (MMft <sup>3</sup> /yr)	111.95					
	Operation (hrs/yr)	8760					
Reference <sup>9</sup>	Potential Emissions*	lbs/hr	tons/yr	lhs/hr	tons/yr	lbs/hr	lons/yr
_	NO <sub>x</sub>	0.20	0.87				
	co	0.34	1.48				
	VOC	10.0	0.04				
	SO <sub>2</sub>	0.00	0.00				
	PM to	0.00	0.01				
	Formaldehyde	0.01	0.03				

<sup>1.</sup>Enter the appropriate Source Identification Number for each natural gas-fitteled reciprocating internal combustion compressor/generator engine located at the compressor station. Multiple compressor engines should be designated CE-1, CE-2, CE-3 etc. If more than three (3) engines exist, please use additional sheets.

2.Enter the Source Status using the following codes:
 NS Construction of New Source (installation) ES Existing Source
 MS Modification of Existing Source RS Removal of Source

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): 10S-PUMP

Name or type and model of proposed affected source: dpiper Diaphragm Pump
On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.
Name(s) and maximum amount of proposed process material(s) charged per hour:
Name(s) and maximum amount of proposed material(s) produced per hour:
Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:

The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

_							
6.	Con	nbustion Data (if applic	able):				
	(a)	Type and amount in ap	propriate units	of fuel(s) to be bu	ırned:		
NA							
	(b) (	Chemical analysis of pr	oposed fuel(s).	excluding coal, ir	ncluding maxim	um percent sulfur	
		and ash:					
NA							
	(c) -	Theoretical combustion	air requiremen	nt (ACF/unit of fue	el):		
		@		°F and		psia.	
						P0.0.	
	(d) F	Percent excess air:					
	(e) 1	Type and BTU/hr of bu	rners and all ot	her firing equipme	ent planned to I	pe used:	
NA							
		· · · · · · · · · · · · · · · · · · ·					
		f coal is proposed as a	source of fuel,	identify supplier a	and seams and	give sizing of the	
NA	(	coal as it will be fired:				:	
1 17 (							
	(g) F	Proposed maximum de	sign heat input			× 10 <sup>6</sup> BTU/hr.	
7.	Proj	ected operating schedu	ıle:		1		
Но	urs/D	ay 1	Days/Week	7	Weeks/Year	52	

8.	3. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:					
@	@ °F and					
a.	NO <sub>x</sub>	lb/hr	grains/ACF			
b.	SO <sub>2</sub>	lb/hr	grains/ACF			
C.	CO	lb/hr	grains/ACF			
d.	PM <sub>10</sub>	lb/hr	grains/ACF			
e.	Hydrocarbons	lb/hr	grains/ACF			
f.	VOCs	7.87 lb/hr	grains/ACF			
g.	Pb	lb/hr	grains/ACF			
h.	Specify other(s)		İ			
	HAPs	<sub>0.58</sub> lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

<sup>(2)</sup> Complete the Emission Points Data Sheet.

with the proposed operating parameters. compliance with the proposed emissions lin	and reporting in order to demonstrate compliance Please propose testing in order to demonstrate nits.
MONITORING	RECORDKEEPING
REPORTING	TESTING
	E PROCESS PARAMETERS AND RANGES THAT ARE ISTRATE COMPLIANCE WITH THE OPERATION OF THIS CONTROL DEVICE.
RECORDKEEPING. PLEASE DESCRIBE THE PROF MONITORING.	POSED RECORDKEEPING THAT WILL ACCOMPANY THE
REPORTING. PLEASE DESCRIBE THE PRORECTION OF THE PROPERTY OF T	OPOSED FREQUENCY OF REPORTING OF THE
POLLUTION CONTROL DEVICE.	SSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR
10. Describe all operating ranges and mainte maintain warranty	nance procedures required by Manufacturer to
Maximum 100 PSI, exhaust routed to control dev	ice if/when driven by natural gas.

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): 11S-FC1 THROUGH 8 1. Name or type and model of proposed affected source: FISCHER CONTROL **DVC 6200** Continuous Bleed Pneumatic Controller Low Bleed 2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants. 3. Name(s) and maximum amount of proposed process material(s) charged per hour: NA 4. Name(s) and maximum amount of proposed material(s) produced per hour: NA 5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants: NA

\* The identification number which appears here must correspond to the air pollution control device identification number appearing on the List Form.

6.	Со	mbustion Data (if applic	able):				
	(a)	Type and amount in ap	propriate unit	s of fuel(s	to be bu	urned:	
NA							
	(b)	Chemical analysis of p	roposed fuel(s	), excludin	ig coal, ir	ncluding maxim	ium percent sulfur
NA		and ash:					
	(c)	Theoretical combustion	air requireme	ent (ACF/u	nit of fue	el):	
	` ,			-		,	
		@			F and		psia.
	(d)	Percent excess air:					
	(e)	Type and BTU/hr of bu	rners and all c	ther firing	equipme	ent planned to	be used:
NA	` '	••		J		•	
	(f)	If coal is proposed as a	source of fue	l, identify s	supplier a	and seams and	give sizing of the
NA		coal as it will be fired:					
							1
	(g)	Proposed maximum de	sign heat inpu	ıt:			× 10 <sup>6</sup> BTU/hr.
7.	Pro	jected operating sched	ule:				
		Day 24	Days/Week	7		Weeks/Year	52
1100	ai 3/1	Juy 21	Daysinger	,		AACCUSI LCUI	UZ

8.	. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:					
@	°F and p					
a.	NO <sub>x</sub>	lb/hr	grains/ACF			
b.	SO <sub>2</sub>	lb/hr	grains/ACF			
C.	СО	lb/hr	grains/ACF			
d.	PM <sub>10</sub>	lb/hr	grains/ACF			
e.	Hydrocarbons	lb/hr	grains/ACF			
f.	VOCs	2.46 lb/hr	grains/ACF			
g.	Pb	lb/hr	grains/ACF			
h.	Specify other(s)					
	HAPs	0.20 lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

<sup>(2)</sup> Complete the Emission Points Data Sheet.

<ol> <li>Proposed Monitoring, Recordkeeping, Report Please propose monitoring, recordkeeping, with the proposed operating parameters. Compliance with the proposed emissions line</li> </ol>	and reporting in order to demonstrate compliance Please propose testing in order to demonstrate
MONITORING	RECORDKEEPING
REPORTING	TESTING
	E PROCESS PARAMETERS AND RANGES THAT ARE
PROCESS EQUIPMENT OPERATION/AIR POLLUTION	
<b>RECORDKEEPING.</b> PLEASE DESCRIBE THE PROFMONITORING.	POSED RECORDKEEPING THAT WILL ACCOMPANY THE
<b>REPORTING.</b> PLEASE DESCRIBE THE PRORECORDKEEPING.	DPOSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMIS POLLUTION CONTROL DEVICE.	SSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR
10. Describe all operating ranges and mainter	nance procedures required by Manufacturer to
maintain warranty	
< 6SCF/hr	

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): 11S-BP

FISO DV0 Con	Name or type and model of proposed affected source: CHER CONTROL C 6200 Itinuous Bleed Pneumatic Controller Bleed
2.	On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.
3. NA	Name(s) and maximum amount of proposed process material(s) charged per hour:
4. NA	Name(s) and maximum amount of proposed material(s) produced per hour:
5. NA	Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
*	The identification number which appears here must correspond to the air pollution control

device identification number appearing on the List Form.

6.	Cor	mbustion Data (if applic	able):			
	(a)	(a) Type and amount in appropriate units of fuel(s) to be burned:				
NA						
_	(h)	Chemical analysis of pr	roposed fuel(s)	evoluding coal in	ocludina maxim	um percent sulfur
		and ash:	oposed idei(s),	, excluding coal, ii	icidaning maxim	an percent sanar
NA						
:	(c)	Theoretical combustion	n air requiremer	nt (ACF/unit of fue	el):	
		@		°F and		psia.
	(d)	Percent excess air:				
	(e)	Type and BTU/hr of bu	rners and all ot	her firing equipme	ent planned to I	be used:
NA						
						-
		If coal is proposed as a coal as it will be fired:	source of fuel,	identify supplier a	and seams and	give sizing of the
NA		oodi do it wiii bo iii od.				
	(g) Proposed maximum design heat input: × 10 <sup>6</sup> BTU/hr.					
7.	Pro	ected operating schedu	ıle:			
Hoi	urs/[	Day 24	Days/Week	7	Weeks/Year	52

8.	3. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:					
@	@ °F and psia					
a.	NO <sub>x</sub>	lb/hr	grains/ACF			
b.	SO <sub>2</sub>	lb/hr	grains/ACF			
c.	CO	lb/hr	grains/ACF			
d.	PM <sub>10</sub>	lb/hr	grains/ACF			
e.	Hydrocarbons	lb/hr	grains/ACF			
f.	VOCs	0.31 lb/hr	grains/ACF			
g.	Pb	lb/hr	grains/ACF			
h.	Specify other(s)					
	HAPs	<sub>0.02</sub> lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

<sup>(2)</sup> Complete the Emission Points Data Sheet.

<ol> <li>Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.</li> </ol>				
MONITORING	RECORDKEEPING			
REPORTING	TESTING			
MONITORING PLEASE LIST AND DESCRIBE THE	E PROCESS PARAMETERS AND RANGES THAT ARE			
	STRATE COMPLIANCE WITH THE OPERATION OF THIS			
	OSED RECORDKEEPING THAT WILL ACCOMPANY THE			
MONITORING.	OCCURED ON DIVERSION AND THE			
REPORTING. PLEASE DESCRIBE THE PRO	POSED FREQUENCY OF REPORTING OF THE			
RECORDKEEPING.				
<b>TESTING.</b> PLEASE DESCRIBE ANY PROPOSED EMIS POLLUTION CONTROL DEVICE.	SSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR			
10. Describe all operating ranges and mainten	nance procedures required by Manufacturer to			
maintain warranty				
< 6SCF/hr				

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): 11S-LC1 THROUGH 16

KIM	Name or type and model of proposed affected source:  KIMRAY SEPARATOR LEVEL CONTROLLER  SENTING SOUTH SERVICE CONTROLLER					
	N II LEVEL CONTROLLER ERMITENT BLEED					
UNI	ENWITERT DEED					
2.	On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.					
3. NA	Name(s) and maximum amount of proposed process material(s) charged per hour:					
4. NA	Name(s) and maximum amount of proposed material(s) produced per hour:					
INM						
5. NA	Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:					
	·					

The identification number which appears here must correspond to the air pollution control device identification number appearing on the List Form.

6.	Combu	stion Data (if applic	able):			
	(a) Typ	e and amount in ap	propriate units	of fuel(s) to be bu	ırned:	
NA						
		emical analysis of p	roposed fuel(s)	, excluding coal, ir	ncluding maxim	um percent sulfur
NA	and	dash:				
	(c) The	eoretical combustion	n air requireme	nt (ACF/unit of fue	el):	
		@		°F and		psia.
	(d) Pei	cent excess air:			***	
	(e) Typ	e and BTU/hr of bu	rners and all ot	her firing equipme	ent planned to I	be used:
NA						
	(f) If c	oal is proposed as a	source of fuel,	identify supplier a	and seams and	give sizing of the
NIA.	COS	l as it will be fired:				
NA						
	(g) Pro	posed maximum de	esign heat input	<u>.</u> :		× 10 <sup>6</sup> BTU/hr.
7.	Proiect	ed operating sched	ule:			
	-			7	ModerNess	50
Ho	urs/Day	24	Days/Week	7	Weeks/Year	52

Page 2 of 4

8.	. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:					
@	@ °F and p					
a.	NO <sub>x</sub>	lb/hr	grains/ACF			
b.	SO₂	lb/hr	grains/ACF			
c.	СО	lb/hr	grains/ACF			
d.	PM <sub>10</sub>	lb/hr	grains/ACF			
e.	Hydrocarbons	lb/hr	grains/ACF			
f.	VOCs	0.01 lb/hr	grains/ACF			
g.	Pb	lb/hr	grains/ACF			
h.	Specify other(s)					
	HAPs	0.20 lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			
		lb/hr	grains/ACF			

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

<ol> <li>Proposed Monitoring, Recordkeeping, Reporting, and Testing         Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.     </li> </ol>				
MONITORING F	RECORDKEEPING			
•				
REPORTING T	ESTING			
MONITORING, PLEASE LIST AND DESCRIBE THE	PROCESS PARAMETERS AND RANGES THAT ARE			
PROPOSED TO BE MONITORED IN ORDER TO DEMONST PROCESS EQUIPMENT OPERATION/AIR POLLUTION CO	TRATE COMPLIANCE WITH THE OPERATION OF THIS			
<b>RECORDKEEPING.</b> PLEASE DESCRIBE THE PROPOSITION OF	SED RECORDKEEPING THAT WILL ACCOMPANY THE			
REPORTING. PLEASE DESCRIBE THE PROPIRECORDICEPING.	OSED FREQUENCY OF REPORTING OF THE			
TESTING. PLEASE DESCRIBE ANY PROPOSED EMISS	NONS TESTING FOR THIS PROCESS FOUIPMENT/AIR			
POLLUTION CONTROL DEVICE.	NOTO PESTINO, ON THIS PROCESS EACH MENTALL			
10. Describe all operating ranges and maintenance procedures required by Manufacturer to				
maintain warranty				
0.00.005/bir				
0.02 SCF/hr				

#### ATTACHMENT M

Air Pollution Control Device Sheets

## Attachment M Air Pollution Control Device Sheet

(FLARE SYSTEM)

Control Device ID No. (must match Emission Units Table): 4C-COMB

#### **Equipment Information**

1.	Manufacturer: LEED Fabrication	2. Method: Elevated flare Ground flare	
		Other	
	Model No. LDF 1350	Describe	
	25. 1000		
3.	Provide diagram(s) of unit describing capture systecapacity, horsepower of movers. If applicable, state	m with duct arrangement and size of duct, air volu hood face velocity and hood collection efficiency.	ıme,
4.	Method of system used:		
	☐ Steam-assisted ☐ Air-assisted	Pressure-assisted Non-assisted	
5.	Maximum capacity of flare:	6. Dimensions of stack:	
	100 scf/min	Diameter 4	ft.
	6,000 scf/hr	Height 25	ft.
7.	Estimated combustion efficiency:	8. Fuel used in burners:	
	(Waste gas destruction efficiency)  Estimated: 99 %	Natural Gas	
	Estimated.	☐ Fuel Oil, Number	
1	Minimum guaranteed: 99 %	Other, Specify:  11. Describe method of controlling flame:	
9.	Number of burners: 1	NA	
	Rating: 11.7 BTU/hr		
10.	Will preheat be used? ☐ Yes ■ No		
12.	Flare height: 25 ft	14. Natural gas flow rate to flare pilot flame per	
40		light: NSCR scf/mi	
13.	Flare tip inside diameter: ft	12.5 scf/hr	
15.	Number of pilot lights: 1	16. Will automatic re-ignition be used?	
	Total 15,000 BTU/hr	Yes No	
	If automatic re-ignition will be used, describe the me	hod:	
piez	zoelectric igniter		
18.	Is pilot flame equipped with a monitor?	□ No	
		-Red	
		era with monitoring control room	
	Other, Describe:		
_			
19.	Hours of unit operation per year: 8760		

#### Steam Injection

				-		
20.	Will steam injection be use	d? Yes	No No	21.	Steam pressure	PSIG
					Minimum Expected:	
22.	Total Steam flow rate:		LB/hr	23.	Temperature:	°F
24.	Velocity		ft/sec	25.	Number of jet streams	
26.	Diameter of steam jets:		in	27.	Design basis for steam in	-
28	How will steam flow be con	trolled if steam	injection is	LISE		B steam/LB hydrocarbon
	THE THE SCOUNT NOT DO CON	nonou a otourr	,001/01/10	abc		
	Ch	orootoricties of	f the Mast	۰.G	as Stream to be Burned	
29.		Quan		- G	Quantity	
	Name	Grains of H			(LB/hr, ft <sup>3</sup> /hr, etc)	Source of Material
	Storage Tank, TL Vapor	NA		1	0.52 lb/hг	Tanks and Loading Vapor
	<del></del>					
				$\top$		
į						
30.	Estimate total combustible	to flare:			LB/hi	r or ACF/hr
	(Maximum mass flow rate of waste gas)				scfm	
31.	Estimated total flow rate to	_	naterials to	be	burned, carrier gases, au	xiliary fuel, etc.:
L	10.52 lb	LD/III	or ACF/hr			
32. NA	Give composition of carrier	gases:				
	72					
33.	Temperature of emission st	tream:		34.	Identify and describe all	auxiliary fuels to be burned.
	TBD	°F				BTU/scf
ŀ	Heating value of emission s	stream: BTU/ft <sup>3</sup>				BTU/scf
	Mean molecular weight of e		<sub>:</sub> .			BTU/scf
	MW = 21.85 lb/lb-m		''			BTU/scf
35.	Temperature of flare gas: 7	70 °F		36.	Flare gas flow rate: 6,00	00 scf/min
37.	Flare gas heat content: 195	50 BTU/ft <sup>3</sup>		38.	Flare gas exit velocity:	ft/sec
39.	Maximum rate during emer	gency for one m	najor piece	of e	equipment or process unit	: NA scf/min
	Maximum rate during emer					
41.	Describe any air pollution reheating, gas humidification		inlet and o	utle	t gas conditioning proces	ses (e.g., gas cooling, gas
42.	Describe the collection mat	terial disposal sy	ystem:			
12	Have you included Flare C	antrol Douise is	n the Emice	cion	e Bointe Data Summany	Shoot?

44. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.					
MONITORING:		RECORDKEEPING:			
Periodic visible em	ission monitoring per regulation.	Pilot records			
DEDODTING		TECTING			
REPORTING:		TESTING:			
In accordance with	regulation(s).	In accordance with regulation(s).			
MONITORING:	Please list and describe the pro-	ocess parameters and ranges that are proposed to be strate compliance with the operation of this process			
	equipment or air control device.				
RECORDKEEPING: REPORTING:	Please describe the proposed re-	cordkeeping that will accompany the monitoring. emissions testing for this process equipment on air			
	pollution control device.				
TESTING:	Please describe any proposed pollution control device.	emissions testing for this process equipment on air			
45. Manufacturer's Gua	aranteed Capture Efficiency for ea	ch air pollutant.			
100%					
46. Manufacturer's Gua	aranteed Control Efficiency for each	h air pollutant.			
98%	•				
47. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty.					
47. Describe all operat	ing ranges and maintenance proce	edures required by Manufacturer to maintain warranty.			

## Attachment M Air Pollution Control Device Sheet

(FLARE SYSTEM)

Control Device ID No. (must match Emission Units Table): 6C-FL

Equipment Information

#### Method: Elevated flare 1 Manufacturer: National Oilwell Varco Ground flare Other Model No. Describe Produced Gas Flare 3. Provide diagram(s) of unit describing capture system with duct arrangement and size of duct, air volume, capacity, horsepower of movers. If applicable, state hood face velocity and hood collection efficiency. 4. Method of system used: Non-assisted Pressure-assisted ☐ Steam-assisted ☐ Air-assisted Dimensions of stack: 5. Maximum capacity of flare: 729.17 Diameter 0.25 ft. scf/min 43,750 20.17 ft. scf/hr Height 8. Fuel used in burners: 7. Estimated combustion efficiency: (Waste gas destruction efficiency) Natural Gas 99 Estimated: % Fuel Oil, Number 98 Other, Specify: % Minimum guaranteed: 11. Describe method of controlling flame: 9. Number of burners: Adjust manual choke upstream of unloading vessel to MM BTU/hr Rating: regulate pressure. No 10. Will preheat be used? Yes 14. Natural gas flow rate to flare pilot flame per pilot 22.67 ft 12. Flare height: scf/min light: **NSCR** 0.33 13. Flare tip inside diameter: ft scf/hr 16. Will automatic re-ignition be used? 15. Number of pilot lights: ☐ Yes No 264.000 BTU/hr Total 17. If automatic re-ignition will be used, describe the method: NA - Flare is only operational while personnel are present and routing stream to vessel. ☐ No 18. Is pilot flame equipped with a monitor? Yes If yes, what type? Thermocouple ☐ Infra-Red ☐ Camera with monitoring control room ☐ Ultra Violet Other, Describe: 19. Hours of unit operation per year: 365

#### Steam Injection

20.	Will steam injection be use	d? 🔲 Yes	No No	21.	Steam pressure Minimum Expected:		PSIG
22.	Total Steam flow rate:		LB/hr	23.	Temperature:		°F
24.	Velocity		ft/sec	25.	Number of jet streams		
26.	Diameter of steam jets:		in	27.	Design basis for steam i	njected: _B steam/LB hy	/drocarbon
28.	How will steam flow be con						
	Ch			te G	as Stream to be Burned		
29.	Name	Quant Grains of H <sub>2</sub>			<b>Quantity</b> (LB/hr, ft <sup>3</sup> /hr, etc)	Source o	f Material
	Well Unloading Gas	NA		2	2320 lb/hr	Wellhead	
				_			
				_			
				_			
30.	Estimate total combustible	to flare:	20 lb/hr		LB/h	r or ACF/hr	
31	(Maximum mass flow rate of Estimated total flow rate to	of waste nas)	natoriale to	o be	burned carrier gases at		
31.	2320 lb/	1)	or ACF/hr		burned, carrier gases, ac	iniliary rues, etc	••
32.	Give composition of carrier						
NA							
33.	Temperature of emission s			34. Identify and describe all auxiliary fuels to be burned.			
	TBD Heating value of emission s	°F stream:					BTU/scf BTU/scf
	1150	BTU/ft <sup>3</sup>					BTU/scf
	Mean molecular weight of e						BTU/scf
_	MW = Ib/lb-m			_	720	47	
$\vdash$	Temperature of flare gas:	°F BTU/ft³		36. Flare gas flow rate: 729.17 scf/min  38. Flare gas exit velocity: 12.4 ft/sec			
	Flare gas heat content:  Maximum rate during emer		aior piece				/min
_				-			U/min
	<ol> <li>Maximum rate during emergency for one major piece of equipment or process unit: NA BTU/min</li> <li>Describe any air pollution control device inlet and outlet gas conditioning processes (e.g., gas cooling, gas reheating, gas humidification):</li> </ol>						
42.	Describe the collection mat	erial disposal sy	stem:				
43	Have you included Flare C	ontrol Device in	the Emis	ssior	is Points Data Summary	Sheet?	
	you moladed reare e						

44. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.					
MONITORING:	o invito	RECORDKEEPING:			
Personnel monitori	ing at all times when flare is opera	Track volume of gas flowed to flare.			
REPORTING:		TESTING:			
In accordance with	regulation(s).	In accordance with regulation(s).			
MONITORING:		ocess parameters and ranges that are proposed to be trate compliance with the operation of this process			
	equipment or air control device.				
RECORDKEEPING: REPORTING:	Please describe any proposed	cordkeeping that will accompany the monitoring. emissions testing for this process equipment on air			
TESTING:	pollution control device.  Please describe any proposed pollution control device.	emissions testing for this process equipment on air			
45. Manufacturer's Gua	aranteed Capture Efficiency for each	ch air pollutant.			
100 %					
	aranteed Control Efficiency for eac	h air pollutant.			
98%					
47. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty.					
125 psig Max. inlet pres					

## AIR POLLUTION CONTROL DEVICE (OTHER COLLECTORS)

Control Device ID No. (must match Emission Units Table): 9C-GEN CAT

	Equipme	ent Information	
1. Manufacturer: TBD		Control Device     Name:	9C-GEN CAT
		Type:	NSCR Catalyst
Provide diagram(s) of unit des horsepower of movers. If applicate			and size of duct, air volume, capacity, efficiency.
4. On a separate sheet(s) supply a	Ill data and calculations	used in selecting or des	igning this collection device.
5. Provide a scale diagram of the	control device showing	internal construction.	
6. Submit a schematic and diagrar	n with dimensions and	flow rates.	
7. Guaranteed minimum collection	efficiency for each poll	utant collected: 100%	
8. Attached efficiency curve and/or	r other efficiency inform	ation.	
9. Design inlet volume: SCFM		10. Capacity:	
11. Indicate the liquid flow rate and	d describe equipment p	rovided to measure press	sure drop and flow rate, if any.
12. Attach any additional data in	cluding auxiliary equip	N/A ment and operation deta	ails to thoroughly evaluate the control
equipment, N/A		mont and operation det	and to moroughly ovalidate the domest
13. Description of method of hand	ling the collected mater	ial(s) for reuse of disposa	ıl. N/A
	Gas Stream	n Characteristics	
14. Are halogenated organics pres	sent? Yes No		
Are particulates present?	☑ Yes ☐No		
Are metals present?	☐ Yes ☑No		
15. Inlet Emission stream parameters:	Max	cimum	Typical
Pressure (mmHg):	Not S	pecified	
Heat Content (BTU/scf):	1	400	1220
Oxygen Content (%):	Not S	pecified	
Moisture Content (%):	Not S	pecified	
Relative Humidity (%):	Not S	pecified	

16. Type of pollutant(s) controlled: SO <sub>x</sub> Odor				
Particulate (type): Other NOx				
17. Inlet gas velocity: TBD ft/sec	18. Pollutant specific gravity: N/A			
19. Gas flow into the collector:	20. Gas stream temperature:			
ACF @ °F and PSIA Inlet: °F				
	Outlet: 960 °F			
21. Gas flow rate:	22. Particulate Grain Loading in grains/scf: N/A			
Design Maximum: ACFM	Inlet:			
Average Expected: ACFM	Outlet:			

23. Emission rate of each pollutant (specify) into and out of collector:

Pollutant	IN P	ollutant	Emission Capture Efficiency	OUT Po	llutant	Control Efficiency	
	lb/hr	grains/acf	%	lb/hr	grains/acf	%	
A NOx	0.99		100	0.20		80	
B VOC	0.34		100	0.34		0	
ссо	0.81		100	0.34		58	
D							
E							

24. Dimensions of stack: Height ft. Diameter ft.

25. Supply a curve showing proposed collection efficiency versus gas volume from 25 to 130 percent of design rating of collector.

#### Particulate Distribution

26. Complete the table:	Particle Size Distribution at Inlet to Collector	Fraction Efficiency of Collector
Particulate Size Range (microns)	Weight % for Size Range	Weight % for Size Range
0-2	N/A	
2 – 4		
4 – 6		
6 – B		
8 – 10		
10 – 12		
12 – 16		
16 – 20		
20 – 30		
30 – 40		
40 – 50		
50 - 60		
60 – 70		
70 – 80		
80 – 90		
90 – 100		
>100		

27. Describe any air pollution control device inlet and out gas humidification): N/A	let gas conditioning processes (e.g., gas cooling, gas reheating,					
28. Describe the collection material disposal system: Ca not disposed of on site.	italyst elements сал be cleaned and/or replaced; materials are					
29. Have you included Other Collectors Control Device	in the Emissions Points Data Summary Sheet?					
30. Proposed Monitoring, Recordkeeping, Reporting,	and Testing					
	ting in order to demonstrate compliance with the proposed demonstrate compliance with the proposed emissions limits.					
MONITORING:	RECORDKEEPING: All maintenance records will be maintained.					
REPORTING: All required emissions test reports will be TESTING: All testing requirements will be performed to ensure submitted to appropriate agencies catalyst performance.						
MONITORING: Please list and describe the process parameters and ranges that are proposed to be monitored in order to demonstrate compliance with the operation of this process equipment or air control device.						
RECORDKEEPING: Please describe the proposed recordkeeping that will accompany the monitoring.						
REPORTING: Please describe any proposed emissions to	esting for this process equipment on air pollution control device.					
TESTING: Please describe any proposed emissions testing	ng for this process equipment on air pollution control device.					
31. Manufacturer's Guaranteed Control Efficiency for each	n air pollutant.					
32. Manufacturer's Guaranteed Control Efficiency for each	n air pollutant.					
33. Describe all operating ranges and maintenance proce	dures required by Manufacturer to maintain warranty.					
See NGSG operations and maintenance plan submitted w	vith the permit application.					

ENGINE MODEL:	C-106
Rich/Lean Burn	Rich
2 or 4 Cycle	4
Bore	7.50
Stroke	8.50
Displacement (CI.)	376
No. Cylinders	1
RPM Max/Min.	800/400
Max HP (cont.)	32
BMEP	84
BSFC (BTU/HP-HR)	10350
Exhaust Stack	
NPT Dia. (in.)	2 1/2"
Height (in.) **	n11"
Temp. (Deg. F)	1302
Flow (acfm)	213
Emissions (g/hp-hr)	
Pre-Cat Nox	14
Pre-Cat CO	11.5
Pre-Cat VOC	N/A
Pre-Cat HCHO	N/A
Post Cat Nox	*2.8
Post Cat CO	*4.8
Post Cat VOC	N/A
Post Cat HCHO	N/A
Max. Exhaust Back	20
Pressure ("W.C.)	
Weight (lb.)Dry (PU)	2690

Noble Energy, Inc. SHL 22 Production Facility

#### ATTACHMENT N

Supporting Emissions Calculations

Noble Energy, Inc; SHL 22 Production Facility Tank Detail Sheet

	0.01846 lb/bbl VOC from FESCO Flash Study 000560 lb/bbl BTEX from FESCO Flash Study d i.good (eg. light brown, good) good (eg. white, fair)	Vent to VDU	Source of Emission Factor Control
I: 8,760 hr/yr 5,600 bbl/day 2,044,000 bbl/yr 33,726 bbl oil/yr	0.01846 lb/bbl VOC from FESCO Flash Study 0.000560 lb/bbl BTEX from FESCO Flash Study Welded (Welded, Bolted, Fiber Green, good (eg. light brown, good) Green, good (eg. white, fair) N/A N/A	0.03 +/- psig 98% %	Estimated Uncontrolled Emissions¹ b/hr) (tpy) (lb/yr)
Source Location Zone: Horizontal: Vertical: Potential operation Potential water production Potential water production	Emission Factor Tank Construction Roof color & condition shell color & condition FR Primary Seal FR Seconday Seal	Vent pressure setting VOC Control Efficiency	Hrs of Estimat Operation (Ib/hr)
1S-TK1-4 400 bbi Produced Water Tanks Produced Water Storage 400 bbi	Produced Water Vent to VDU Vertical, above ground 20 ft 12 ft 0.06		CAS
Source ID Number Equipment ID Tank Description Tank Usage Tank Make Tank Capacity Serial Number Date in Service	Tank Contents Produ Emission Controls Tank Orientation Vertics Shell Height / Length Shell Diameter Roof Slope Roof Type (Cone, Dome, IFR, Cone EFR, None)	Permit Status Potential Emissions	Pollutant

VOC-Flash VOC-W&B Total VOC Total HAPs

37,732 FESCO Flash Summary 13,139 TANKS 4.0.9d

18.87 6.57 **25.44** 3.214

4.31 1.50 5.81 0.734

<sup>&</sup>lt;sup>1</sup>Emissions include working and breathing \*Assumes 1.65% oil in PW

Noble Energy, Inc; SHL 22 Production Facility Produced Water Truck Loadout

Source ID Number	2S-TL1	Location	NZF
Source Description Source Usage	Produced Water Truck Loadout Produced Water Truck Loadout		536119.556 4428832.49
			39.9957662
Potential operation	8,760	Longitiude	ongitiude -80.560996
Capture Efficiency	20%		
Control Efficiency	98%		
HAP Speciation			
BTEX	2.40% wt% of VOC E	Based on FESCO PW str	Based on FESCO PW study; ratio of lb BTEX/bbl to lb VOC/bbl of PW
Total HAPs	20.96% wt% of VOC		

Potential Emissions										
Pollutant	EPA	True VP	Mol. Wt.	Tof	ö	Estir	Estimated Emissions	ns	Source of	
	S Factor	of Liquid	of Vapors⁴	Liquid <sup>5</sup>	Volume				Emission	Notes
		(bsia)	(lp/lp-mol)	(R)	(bbl/yr) <sup>2</sup>	(lb/1000 gat)	(lb/hr)	(tpy)	Factor	
VOC	0.6	12.00	64	530	33,726	10.83		2.30	AP-421	ATMOSPHERE
HAPs							0.00	0.48	AP-421	ATMOSPHERE
VOC	9.0	12.00	64	530	33,726	10.83	1.23	5.37	AP-421	To VDU
HAPs							0.00	1.13	AP-421	To VDU
voc	9.0	12.00	64	530	33,726	10.83	0.02	0.11	AP-421	Controlled
HAPs							0.00	0.02	AP-421	Controlled

EPA AP-42, Volume I, Fifth Edition - January 1995, Table 5.2-1, Saturation (S) Factors for Calculating Petroleum Liquid Loading Losses

Controlled

<sup>&</sup>lt;sup>2</sup>The oil volume for this calculation assumes that 1,65% of the produced water volume is oil.

<sup>&</sup>lt;sup>3</sup>EPA AP-42, Volume I, Fifth Edition - January 1995, Section 5.2.2.1.1. Assumes a minimum collection efficiency of 70%. <sup>4</sup>Molecular Weight of Vapors comes from TANKS4.0.9 run, Liquid Contents of Storage Tank table

Temperature comes from HYSYS run, "Water Out" stream

ARROW C-106	9S-GEN	32 hp	ď	800 RPM			
Fuel Heat Value		1220	1220 Btu/scf				
Heat Rate		0.3312	0.3312 MMBtu/hr				
Engine Heat Rate		10350	10350 Btu/hp-hr				
Control		NSCR					
Pollutant	Emission Factor	actor	Nominal	Hrs of	Estimated Emissions	ons	Source of Pollutant
			Rating	Operation		ш	Emission Factor
	(Ib/MMBtu)	(g/hp-hr)	(hp)	(hrs/yr)	(lb/hr)	(tpy)	
NOX		2.80	32	8760	0.20	0.87	Mfr Factors NOx
00		4.80	32	8760	0.34	1.48	Mfr Factors CO
,,oc	2.96E-02		32	8760	0.01	0.04	AP-42 Ch. 3.2, table 3.2-3
CO2	110		32	8760	36.43	159.57	AP-42 Ch. 3.2, table 3.2-3
SOx	5.88E-04		32	8760	0.00	0.00	AP-42 Ch. 3.2, table 3.2-3
μd	9.50E-03		32	8760	0.00	0.01	AP-42 Ch. 3.2, table 3.2-3
PM10	9.50E-03		32	8760	0.00	0.01	AP-42 Ch. 3.2, table 3.2-3
Formaldehyde	2.05E-02		32	8760	0.01	0.03	AP-42 Ch. 3.2, table 3.2-3
Benzene	1.58E-03		32	8760	0.00	0.00	AP-42 Ch. 3.2, table 3.2-3
Toluene	5.58E-04		32	8760	0.00	00.0	AP-42 Ch. 3.2, table 3.2-3
Ethylbenzene	2.48E-05		32	8760	0.00	0.00	AP-42 Ch. 3.2, table 3.2-3
Xylene	1.95E-04		32	8760	0.00	00.0	AP-42 Ch. 3.2, table 3.2-3
Ť.	0.23		32	8760	0.08	0.33	API
CO <sub>2</sub> e						167.91	
API Compendium of Greenhouse Gas Emissions Methodoligies for the Oil and Natural Gas Industry, Table 4-9	Gas Emissions Methodoli	gies for the Oil	and Natural (	3as Industry, Table 4-9			
<sup>2</sup> Includes total hydrocarbons							
Notes							

### Noble Energy, Inc; SHL 22 Production Facility Heater Detail Sheet

			-	 	,
Source ID Number	3S-GPU1		- !		
Equipment ID	3S-GPU1				
SCC					
Emission Unit Description	GPU Burner	•			
Equipment Usage	GPU Heate	r	1		
Equipment Make	Unknown		- 1		
Equipment Model	Unknown		- 1		
Serial Number	Unknown				
Installation Date	NEW CONS	ST.			
Emission Controls	None				
Fuel Heating Value	4000	Dhulaaf			
Fuel Heating Value	1200	Btu/scf	ŀ		
Design Heat Rate*	2.00	MMBtu/hr	- [		
Site Heat Rate*	2.00	MMBtu/hr			
Potential Operation	8760	hr/yr			
Potential Fuel Usage	14.60	MMscf/yr			

<sup>\*</sup> These are heat release rates and not the duty for the heater

#### Potential Emissions

Pollutant	Emission	Nominal	Hrs of	Estimated E	Emissions	Source of
	Factor	Rating	Operation			Emission
	(lb/MMscf)	(MMBtu/hr)	(hrs/yr)	(lb/hr)	(tpy)	Factor
NOx	100.00	2.000	8760	0.17	0.73	AP-42 <sup>1</sup>
co	84.00	2.000	8760	0.14	0.61	AP-421
voc	5.50	2.000	8760	0.01	0.04	AP-42 <sup>2</sup>
SO2	0.60	2.000	8760	0.00	0.00	AP-42 <sup>2</sup>
PM10	7.60	2.000	8760	0.01	0.06	AP-42 <sup>2</sup>
Formaldehyde	0.08	2.000	8760	0.00	0.00	AP-42 <sup>3</sup>
Total HAPs	1.89	2.000	8760	0.00315	0.01	AP-42 <sup>3</sup>
CO₂	120000.00	2.000	8760	200.00	876.00	AP-42 <sup>2</sup>
СН₄	2.30	2.000	8760	0.00	0.02	AP-42 <sup>2</sup>
CO <sub>2</sub> e					876.42	

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-1, Emission Factors for Nitrogen Oxides (NOx) and Carbon Monoxide (CO) from Natural Gas Combustion

<sup>&</sup>lt;sup>2</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-2, Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion

<sup>&</sup>lt;sup>3</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-3, Emission Factors for Speciated Organic Compounds from Natural Gas Combustion

Source ID Number	3S-GPU2		
Equipment ID	3S-GPU2		
scc			
Emission Unit Description	<b>GPU Burner</b>		
Equipment Usage	<b>GPU Heater</b>		
Equipment Make	Unknown		
Equipment Model	Unknown		
Serial Number	Unknown		
Installation Date	<b>NEW CONST.</b>	a a	
Emission Controls	None		
Fuel Heating Value	1200	Btu/scf	
Design Heat Rate*	2.00	MMBtu/hr	
Site Heat Rate*	2.00	MMBtu/hr	
Potential Operation	8760	hr/yr	
Potential Fuel Usage	14.60	MMscf/yr	

<sup>\*</sup> These are heat release rates and not the duty for the heater

Pollutant	Emission	Nominal	Hrs of	Estimated	Estimated Emissions	
1	Factor	Rating	Operation			Emission
	(lb/MMscf)	(MMBtu/hr)	(hrs/yr)	(lb/hr)	(tpy)	Factor
NOx	100.00	2.000	8760	0.17	0.73	AP-42 <sup>1</sup>
co	84.00	2.000	8760	0.14	0.61	AP-42 <sup>1</sup>
voc	5.50	2.000	8760	0.01	0.04	AP-42 <sup>2</sup>
SO2	0.60	2.000	8760	0.00	0.00	AP-42 <sup>2</sup>
PM10	7.60	2.000	8760	0.01	0.06	AP-42 <sup>2</sup>
Formaldehyde	0.08	2.000	8760	0.00	0.00	AP-42 <sup>3</sup>
Total HAPs	1.89	2.000	8760	0.00315	0.01	AP-42 <sup>3</sup>
CO₂	120000.00	2.000	8760	200.00	876.00	AP-42 <sup>2</sup>
CH₄	2.30	2.000	8760	0.00	0.02	AP-42 <sup>2</sup>
CO₂e					876.42	

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-1, Emission Factors for Nitrogen Oxides (NOx) and Carbon Monoxide (CO) from Natural Gas Combustion

<sup>&</sup>lt;sup>2</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-2, Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion

<sup>&</sup>lt;sup>3</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-3, Emission Factors for Speciated Organic Compounds from Natural Gas Combustion

Source ID Number	3S-GPU3	
Equipment ID	3S-GPU3	
SCC		
Emission Unit Description	GPU Burner	
Equipment Usage	GPU Heater	
Equipment Make	Unknown	
Equipment Model	Unknown	
Serial Number	Unknown	
Installation Date	NEW CONST	Γ.
Emission Controls	None	
Fuel Heating Value	1200	Btu/scf
Design Heat Rate*	2.00	MMBtu/hr
Site Heat Rate*	2.00	MMBtu/hr
Potential Operation	8760	hr/yr
Potential Fuel Usage	14.60	MMscf/yr

<sup>\*</sup> These are heat release rates and not the duty for the heater

Pollutant	Emission	Nominal	Hrs of	Estimated t	Emissions	Source of
	Factor	Rating	Operation			Emission
	(lb/MMscf)	(MMBtu/hr)	(hrs/yr)	(lb/hr)	(tpy)	Factor
NOx	100.00	2.000	8760	0.17	0.73	AP-421
co	84.00	2.000	8760	0.14	0.61	AP-42 <sup>1</sup>
voc	5.50	2.000	8760	0.01	0.04	AP-42 <sup>2</sup>
SO2	0.60	2.000	8760	0.00	0.00	AP-42 <sup>2</sup>
PM10	7.60	2.000	8760	0.01	0.06	AP-42 <sup>2</sup>
Formaldehyde	0.08	2.000	8760	0.00	0.00	AP-42 <sup>3</sup>
Total HAPs	1.89	2.000	8760	0.00315	0.01	AP-42 <sup>3</sup>
CO₂	120000.00	2.000	8760	200.00	876.00	AP-42 <sup>2</sup>
CH₄	2.30	2.000	8760	0.00	0.02	AP-42 <sup>2</sup>
CO₂e					876.42	

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-1, Emission Factors for Nitrogen Oxides (NOx) and Carbon Monoxide (CO) from Natural Gas Combustion

<sup>&</sup>lt;sup>2</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-2, Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion

<sup>&</sup>lt;sup>3</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-3, Emission Factors for Speciated Organic Compounds from Natural Gas Combustion

3S-GPU4	
3S-GPU4	
<b>GPU Burner</b>	
<b>GPU</b> Heater	
Unknown	
Unknown	
Unknown	
<b>NEW CONST</b>	•
None	
4000	Dt. tt
	Btu/scf
2.00	MMBtu/hr
2.00	MMBtu/hr
8760	hr/yr
14.60	MMscf/yr
	3S-GPU4  GPU Burner GPU Heater Unknown Unknown Unknown NEW CONST None  1200 2.00 2.00 8760

<sup>\*</sup> These are heat release rates and not the duty for the heater

Pollutant	Emission	Nominal	Hrs of	Estimated	Estimated Emissions	
	Factor	Rating	Operation			Emission
	(lb/MMscf)	(MMBtu/hr)	(hrs/yr)	(lb/hr)	(tpy)	Factor
NOx	100.00	2.000	8760	0.17	0.73	AP-42 <sup>1</sup>
co	84.00	2.000	8760	0.14	0.61	AP-42 <sup>1</sup>
voc	5.50	2.000	8760	0.01	0.04	AP-42 <sup>2</sup>
SO2	0.60	2.000	8760	0.00	0.00	AP-42 <sup>2</sup>
PM10	7.60	2.000	8760	0.01	0.06	AP-42 <sup>2</sup>
Formaldehyde	0.08	2.000	8760	0.00	0.00	AP-42 <sup>3</sup>
Total HAPs	1.89	2.000	8760	0.00315	0.01	AP-42 <sup>3</sup>
CO₂	120000.00	2.000	8760	200.00	876.00	AP-42 <sup>2</sup>
CH₄	2.30	2.000	8760	0.00	0.02	AP-42 <sup>2</sup>
CO₂e					876.42	

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-1, Emission Factors for Nitrogen Oxides (NOx) and Carbon Monoxide (CO) from Natural Gas Combustion

<sup>&</sup>lt;sup>2</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-2, Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion

<sup>&</sup>lt;sup>3</sup> EPA AP-42, Volume I. Fifth Edition - July 1998. Table 1.4-3, Emission Factors for Speciated Organic Compounds from Natural Gas Combustion

Source ID Number	3S-GPU5	
Equipment ID	3S-GPU5	
SCC		
Emission Unit Description	GPU Burner	
Equipment Usage	GPU Heate	г
Equipment Make	Unknown	
Equipment Model	Unknown	
Serial Number	Unknown	
Installation Date	NEW CONS	T
Emission Controls	None	
Fuel Heating Value	1200	Btu/scf
Design Heat Rate*	2.00	MMBtu/hr
Site Heat Rate*	2.00	MMBtu/hr
Potential Operation	8760	hr/yr
Potential Fuel Usage	14.60	MMscf/yr
4 4	4 14	1 . 5 41 1 .

<sup>\*</sup> These are heat release rates and not the duty for the heater

Pollutant	Emission	Nominal	Hrs of	Estimated I	Estimated Emissions	
	Factor	Rating	Operation			Emission
	(lb/MMscf)	(MMBtu/hr)	(hrs/yr)	(lb/hr)	(tpy)	Factor
NOx	100.00	2.000	8760	0.17	0.73	AP-42 <sup>1</sup>
co	84.00	2.000	8760	0.14	0.61	AP-42 <sup>1</sup>
voc	5.50	2.000	8760	0.01	0.04	AP-42 <sup>2</sup>
SO2	0.60	2.000	8760	0.00	0.00	AP-42 <sup>2</sup>
PM10	7.60	2.000	8760	0.01	0.06	AP-42 <sup>2</sup>
Formaldehyde	0.08	2.000	8760	0.00	0.00	AP-42 <sup>3</sup>
Total HAPs	1.89	2.000	8760	0.00315	0.01	AP-42 <sup>3</sup>
CO₂	120000.00	2.000	8760	200.00	876.00	AP-42 <sup>2</sup>
CH₄	2.30	2.000	8760	0.00	0.02	AP-42 <sup>2</sup>
CO₂e					876.42	

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-1, Emission Factors for Nitrogen Oxides (NOx) and Carbon Monoxide (CO) from Natural Gas Combustion

<sup>&</sup>lt;sup>2</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-2, Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion

<sup>&</sup>lt;sup>3</sup> EPA AP-42, Volume I. Fifth Edition - July 1998, Table 1.4-3, Emission Factors for Speciated Organic Compounds from Natural Gas Combustion

<sup>\*</sup> These are heat release rates and not the duty for the heater

Potential Emissions						
Pollutant	Emission	Nominal	Hrs of	Estimated I	Estimated Emissions	
	Factor	Rating	Operation			Emission
	(lb/MMscf)	(MMBtu/hr)	(hrs/yr)	(lb/hr)	(tpy)	Factor
NOx	100.00	2.000	8760	0.17	0.73	AP-42 <sup>1</sup>
co	84.00	2.000	8760	0.14	0.61	AP-42 <sup>1</sup>
voc	5.50	2.000	8760	0.01	0.04	AP-42 <sup>2</sup>
SO2	0.60	2.000	8760	0.00	0.00	AP-42 <sup>2</sup>
PM10	7.60	2.000	8760	0.01	0.06	AP-42 <sup>2</sup>
Formaldehyde	0.08	2.000	8760	0.00	0.00	AP-42 <sup>3</sup>
Total HAPs	1.89	2.000	8760	0.00315	0.01	AP-42 <sup>3</sup>
CO <sub>2</sub>	120000.00	2.000	8760	200.00	876.00	AP-42 <sup>2</sup>
CH₄	2.30	2.000	8760	0.00	0.02	AP-42 <sup>2</sup>
CO₂e			-		876.42	

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-1, Emission Factors for Nitrogen Oxides (NOx) and Carbon Monoxide (CO) from Natural Gas Combustion

<sup>&</sup>lt;sup>2</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-2, Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion

<sup>&</sup>lt;sup>3</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-3, Emission Factors for Speciated Organic Compounds from Natural Gas Combustion

			_
Source ID Number	3S-GPU7		
Equipment ID	3S-GPU7		
scc			
Emission Unit Description	GPU Burner		į
Equipment Usage	GPU Heate	r	
Equipment Make	Unknown		
Equipment Model	Unknown		
Serial Number	Unknown		
Installation Date	NEW CONS	iT.	
Emission Controls	None		
Fuel Heating Value	1200	Btu/scf	
Design Heat Rate*	2.00	MMBtu/hr	
Site Heat Rate*	2.00	MMBtu/hr	
Potential Operation	8760	hr/yr	
Potential Fuel Usage	14.60	MMscf/yr	

<sup>\*</sup> These are heat release rates and not the duty for the heater

Pollutant	Emission	Nominal	Hrs of	Estimated	Estimated Emissions	
	Factor	Rating	Operation			Emission
	(lb/MMscf)	(MMBtu/hr)	(hrs/yr)	(lb/hr)	(tpy)	Factor
NOx	100.00	2.000	8760	0.17	0.73	AP-42 <sup>1</sup>
co	84.00	2.000	8760	0.14	0.61	AP-42 <sup>1</sup>
voc	5.50	2.000	8760	0.01	0.04	AP-42 <sup>2</sup>
SO2	0.60	2.000	8760	0.00	0.00	AP-42 <sup>2</sup>
PM10	7.60	2.000	8760	0.01	0.06	AP-42 <sup>2</sup>
Formaldehyde	0.08	2.000	8760	0.00	0.00	AP-42 <sup>3</sup>
Total HAPs	1.89	2.000	8760	0.00315	0.01	AP-42 <sup>3</sup>
CO₂	120000.00	2.000	8760	200.00	876.00	AP-42 <sup>2</sup>
CH₄	2.30	2.000	8760	0.00	0.02	AP-42 <sup>2</sup>
CO₂e					876.42	,

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-1, Emission Factors for Nitrogen Oxides (NOx) and Carbon Monoxide (CO) from Natural Gas Combustion

<sup>&</sup>lt;sup>2</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-2, Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion

<sup>&</sup>lt;sup>3</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-3, Emission Factors for Speciated Organic Compounds from Natural Gas Combustion

Source ID Number	3S-GPU8	
Equipment ID	3S-GPU8	
scc		
Emission Unit Description	<b>GPU Burner</b>	
Equipment Usage	GPU Heater	
Equipment Make	Unknown	
Equipment Model	Unknown	
Serial Number	Unknown	
Installation Date	NEW CONST	Γ.
Emission Controls	None	
Fuel Heating Value	1200	Btu/scf
Design Heat Rate*	2.00	MMBtu/hr
Site Heat Rate*	2.00	MMBtu/hr
Potential Operation	8760	hr/yr
Potential Fuel Usage	14.60	MMscf/yr

<sup>\*</sup> These are heat release rates and not the duty for the heater

Pollutant	Emission	Nominal	Hrs of	Estimated	Emissions	Source of
	Factor	Rating	Operation			Emission
	(lb/MMscf)	(MMBtu/hr)	(hrs/yr)	(lb/hr)	(tpy)	Factor
NOx	100.00	2.000	8760	0.17	0.73	AP-42 <sup>1</sup>
co	84.00	2.000	8760	0.14	0.61	AP-42 <sup>1</sup>
VOC	5.50	2.000	8760	0.01	0.04	AP-42 <sup>2</sup>
SO2	0.60	2.000	8760	0.00	0.00	AP-42 <sup>2</sup>
PM10	7.60	2.000	8760	0.01	0.06	AP-42 <sup>2</sup>
Formaldehyde	0.08	2.000	8760	0.00	0.00	AP-42 <sup>3</sup>
Total HAPs	1.89	2.000	8760	0.00315	0.01	AP-42 <sup>3</sup>
CO₂	120000.00	2.000	8760	200.00	876.00	AP-42 <sup>2</sup>
CH₄	2.30	2.000	8760	0.00	0.02	AP-42 <sup>2</sup>
CO₂e					876.42	

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-1, Emission Factors for Nitrogen Oxides (NOx) and Carbon Monoxide (CO) from Natural Gas Combustion

<sup>&</sup>lt;sup>2</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-2, Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion

<sup>&</sup>lt;sup>3</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-3, Emission Factors for Speciated Organic Compounds from Natural Gas Combustion

#### Noble Energy, Inc; SHL 22 Production Facility

Enclosed	Elara	Dotall	Chast
Eliciosea	Ligie	Detail	Sheet

Source ID Number								
Equipment ID	4S-COM		Truck Loading VOC Emissions & F	Truck Loading VOC Emissions & Flash VRU downtime				
Equipment Usage	Vapor Combustor		Produced Water Tanks	25.44 tov VOC	3.21 toy HAPs			
			Produced Water Loading	5.37 tpy VOC	1.13 tpy HAPs			
Equipment Make	Leed		Total VOC Emissions	30.81 tpy	4.34 tpy HAPs			
Equipment Model	LDF1350	Dual Stage Combustor						
Serial Number	Unknown		Control Efficiency	98%	98%			
Installation Date	02/01/17		Controlled VOC Emissions	0.62 tpy	0.09 tpy HAPs			
Emission Controls	None		Combustion					
Pilot			Molecular Weight of Vapors	lb/lb-mel				
Fuel Heating Value	1200	Btu/scf	Fuel Heating Value	1950 Btu/scf				
Design Heat Rate	G.02	MMBtu/hr	Potential Heat Output	11.700 MMBtu/hr				
Site Heat Rate	0.02	MMBtu/hr	VOC Vapors sent to flare	61613.0 lbs/yr				
Potential Operation	365	days/yr	Potential Operation	365 days/yr				
Potential Fuel Usage	0.30	Mscfiday	Ave. Gas Flared	144.000 Mscf/day				

9S-PILOT1 Combustor Pilot Emissions

COMOGSIG: FINDI EM	113510113					
Pollulant	Emission	Annual gas	Hrs of	Estimated	Emissions	Source of
	Factor	Usage	Operation		Pilot	Emission
	lb/MMSCF	MMSCF/yr	(hrs/yr)	(lb/hr)	tpy	Factor
NOx	100.000	0.11	8760	0.00	0.01	AP-42 <sup>2</sup>
co	84.000	0.11	8760	0.00	0.005	AP-42 <sup>2</sup>
PM10	7.600	0.11	9760	0.00	0.00	AP-42 <sup>2</sup>
voc	5.500	0.11	8760	0.00	0.00	AP-42 <sup>2</sup>
N <sub>2</sub> O	1.000	0.11	8760	0.00	0.00	API
CO <sub>2</sub>	120000.000	0.11	8760	1.50	6.57	AP-42 <sup>2</sup>

Potential Combustion Emissions

1 Olerator Compassion Ethiosophia								
Pollulant	Emission	Annual gas	Estimated	Emission				
	Factor	Usage	Emissions	Factor				
	lb/MMBtu	MMBlu/yr	tpy	Source				
NOx	0.068	102492.00	3.48	AP-421				
co	0.370	102492.00	18.96	AP-421				
N <sub>2</sub> O	0.001	102492.00	0.05	API				
CO2	117.650	102492.00	6029.09	AP-421				

Total Potential Vapor Combustor Emissions

Pollutant	tpy	lb/hr
NOx	3.49	0.80
CO	18.97	4.33
PM10	0.00	0.00
VOC	0.62	0.14
HAPs	0.09	0.02
N₂O	0.05	0.01
CO <sub>2</sub>	6035.66	1378.01
CO₂e	6051.31	1381.58

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - September 1991, Table 13.5-1, Emission Factors for Flare Operations.

<sup>&</sup>lt;sup>2</sup> EPA AP-42, Volume I, Fifth Edition - September 1991, Table 1.4, Emission Factors for Natural Gas Combustion

# Noble Energy, Inc; SHL 22 Production Facility Fuel Cell

Source ID Number	8S-FC	
Equipment ID	8S-FC	
Equipment Usage	Remote Powe	r System
Equipment Make	Acumentrics	
Equipment Model	Propane	
Serial Number	TBD	
Installation Date	<b>NEW CONST</b>	6
Emission Controls	None	
Fuel Heating Value	91600	Btu/gal
Design Heat Rate*	5496	Btu/hr
Site Heat Rate*	0.005496	MMBtu/hr
Potential Operation	8760	hr/yr
Potential Fuel Usage	1.44	gal/day

Pollutant	Emission	Hrs of	Estimated Emissions		Source of
	Factor	Operation			Emission
	(lb/10 <sup>3</sup> gal)	(hrs/yr)	(lb/hr)	(tpy)	Factor
NOx	13.00	8760	7.80E-04	0.00	AP-42 <sup>1</sup>
co	7.50	8760	4.50E-04	0.00	AP-42 <sup>1</sup>
VOC	1.00	8760	6.00E-05	0.00	AP-42 <sup>1</sup>
SO2	0.10	8760	6.00E-06	0.00	AP-42 <sup>1</sup>
PM10	0.70	8760	4.20E-05	0.00	AP-42 <sup>1</sup>
CO <sub>2</sub>	12500.00	8760	7.50E-01	3.29	AP-42 <sup>1</sup>
CH₄	0.20	8760	1.20E-05	0.00	AP-42 <sup>1</sup>
CO₂e				3.29	

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 2008, Table 1.5-1, Emission Factors for LPG Combustion

#### Noble Energy, Inc; SHL 22 Production Facility

Elmen	Datail	Sheet

Fiare Detail Sheet						
Source ID Number	6S-FL					
Equipment (D	6C-FL			voc	HAPs	
Equipment Usage	Unloading	g Vessel Centrol	Unloading Vessel	165.84 tpy	12.1670034 lpy	
	Sandpipe	er Diaphragm Pump Control	Diaphragm Pump	1.44 tpy	0.11 tpy	
Equipment Make	NOV		Total Emissions	167.27 tpy UNCONTROLLED	12.27 tpy	UNCONTROLLED
Equipment Model	Produced	d Gas Flare		908.95 lb/hr UNCONTROLLED	66.69 lb/hr	UNCONTROLLED
Sensi Number	Unknown		Control Efficiency	98%	98%	
Installation Date	02/01/17		Controlled Emissions	3.35 tpy CONTROLLED	0.25 tpy	CONTROLLED
				18.18 lb/hr CONTROLLED	1.33 lb/hr	CONTROLLED
Pilot						
Fuel Heating Value	1220	Btu/scf	Fuel Heating Value	1150 Blu/scf		
Design Heat Rate	0.26	MMBttt/hr	Potential Heat Output	74.727 MMBtu/hr		
Site Heat Rate	0.26	MMBturnr	VOC Vapors sent to flare	334546.0 lbs/vr		
Potential Operation	365	days/yr	Potential Operation	15.20 days/yr		
Potential Fuel Usage	5.19	Mscf/day	MAX. Gas Flared	1559.520 Mscf/day		

Flare Pilot Emissions

Pollutarii	Emission	Annual gas	Hrs of	Esti	mated Emissions	Source of	
	Factor Ib/MMSCF	Usage MMSCF/yr	Operation (hrs/yr)	(lb/hr)	Pilot Ipy	Emission Factor	
NOx	100.000	1.90	8760	0.02	0.09	AP-42 <sup>2</sup>	
CO	84.000	1.90	8760	0.02	0.08	AP-42 <sup>2</sup>	
PM10	7.600	1,90	8760	0.00	0.01	AP-42 <sup>2</sup>	
VOC	5.500	1.90	8760	0.00	0.01	AP-42 <sup>2</sup>	
N₂O	1.000	1,90	8760	0.00	0.00	API	
CO2	120000.000	1.90	8750	25.97	113.74	AP-422	

Unloading Vessel Emissions

arrive training training						
Pollulant	Emission		Hrs of	Estimated	Estimated	Emission
	Factor	Usage	Operation	Emissions	Emissions	Factor
	tb/MMBtu	MMBtu/hr	(hrs/yr)	lb/hr	tpy	Source
NOx	0.068	74.73	365	5.08	0.93	AP-421
co	0.370	74.73	365	27.65	5.04	AP-421
N₂O	0.001	74.73	365	0.08	0.01	API
CO2	117,850	74.73	365	8791.63	1604.02	AP-421

Sandpiper Diaphragm Pump Emissions

Polkulant	Emission		Hrs of	Estimated	Estimaled	Emission
	Factor	Usage	Operation	Emissions	Emissions	Factor
	lb/MMBtu	MMBtu/hr	(hrs/yr)	ltb/hr	lpy	Source
NOx	0.068	1.46	365	0.10	0.02	AP-421
co	0.370	1.45	365	0.54	0.10	AP-421
N <sub>2</sub> O	0.001	1.46	365	0.00	0.00	API
CO2	117.650	1.46	365	172.24	31.42	AP-421

Tatal Potential Vapor Combustor Emissions

Pollutant	tpy	ib/hr
NOx	1.04	5.20
co	5.22	28.21
PM10	0.01	0.00
VOC	3.35	18.34
HAPs	0.25	1.35
N <sub>2</sub> O	0.02	0.08
CH₄	18.08	4.13
ÇO <sub>2</sub>	1749.18	8989.84
CO₂e	2205.67	9116.33

<sup>&</sup>lt;sup>1</sup> EPA AP-42, Volume I, Fifth Edition - September 1991, Table 13.5-1, Emission Factors for Flare Operations.

 $<sup>^4</sup>$  EPA AP-42, Volume I, Fifth Edition - September 1991, Table 1.4, Emission Factors for Natural Gas Combustion

Noble Energy, Inc; SHL 22 Production Facility

Pump Detail Sheet

Source ID Number	10S-Pump			
Equipment ID	Sandpiper Diaphragm Pump			
Equipment Usage	Unloading Vessel Fluid Transfer			
Equipment Make	Sandpiper			
Equipment Model	G20			
Serial Number	Unknown			
Installation Date	02/01/17			
Pilot				
Design Rate	20.00	scf/min		
Potential Operation	365	hours/yr		
Controle Efficeincy	98.00%	%		

Potential Emissions

Pollutant		Estimated Uncon	trolled Emissions	Source of	
				Emission Factor	Control
	wt frac	(lb/hr)	(tpy)		
VOC	1.28E-01	7.87	1.44	HYSYS	6C-FL
Benzene	4.43E-05	0.00	0.00	HYSYS	6C-FL
Toluene	1.05E-04	0.01	0.00	HYSYS	6C-FL
Ethylbenzene	9.96E-06	0.00	0.00	HYSYS	6C-FL
Xylene	6.58E-05	0.00	0.00	HYSYS	6C-FL
n-Hexane	9.18E-03	0.56	0.10	HYSYS	6C-FL
Total HAPs		0.577	0.105	HYSYS	6C-FL
CH4	6.92E-01	42.463	7.747	HYSYS	6C-FL

**Controlled Emissions** 

Pollutant	Estimated Contr	Source of Emission Factor	or Control	
	(lb/hr)	(tpy)		
VOC	0.16	0.03	HYSYS	6C-FL
Benzene	0.00	0.00	HYSYS	6C-FL
Toluene	0.00	0.00	HYSYS	6C-FL
Ethylbenzene	0.00	0.00	HYSYS	6C-FL
Xylene	0.00	0.00	HYSYS	6C-FL
n-Hexane	0.01	0.00	HYSYS	6C-FL
Total HAPs	0.01	0.00	HYSYS	6C-FL
CH4	0.85	0.15	HYSYS	6C-FL

# Noble Energy, Inc. SHL 22 Production Facility Pneumatic Controllers

Equipment ID	11S-FC1	-8, 11S-BP		
Equipment Usage	Flow Control / Back Pressure			
Equipment Make	Fischer Control			
Equipment Model	DVC 620	0		
Emission Controls	None			
Equipment Count	9			
Design Flow*	6.00	SCFH		
Potential Operation	8760	hr/yr		
Service	NG	•		

Equipment ID	11S-LC	1-16	
Equipment Usage	Separator Level Control		
Equipment Make	KIMRAY		
Equipment Model	GEN II I	evel Controllers	
Emission Controls	None		
Equipment Count	16		
Design Flow*	0.02	SCFH	
Potential Operation	8760	hr/yr	
Service	NG	-	

Potential Emissions 11S-FC1-8

Pollutant		Emission	Hrs of	Estimated Emi	ssions	Source of
1		Factor	Operation			Emission
	% of VOC	(lb/SCF)	(hrs/yr)	(lb/hr)	(tpy)	Factor
VOC		0.05	8760	2.46	10.76	Gas Analysis
n-Hexane	7.80E-02			0.19	0.84	HYSYS % of VOC
Benzene	1.70E-04			0.00	0.00	HYSYS % of VOC
Toluene	7.23E-04		1	0.00	0.01	HYSYS % of VOC
Ethylbenzene	9.26E-05			0.00	0.00	HYSYS % of VOC
Xylenes	6.95E-04			0.00	0.01	HYSYS % of VOC
Total HAPs	7.34E-02		8760	0.20	0.86	HYSYS % of VOC
CH4	5.40E+00			13.25	58.04	HYSYS % of VOC

Potential Emissions 11S-BP

r Oterniar Emissions	TTO-DF					
Pollutant		Emission	Hrs of	Estimated Emis	sions	Source of
1		Factor	Operation			Emission
	% of VOC	(lb/SCF)	(hrs/yr)	(lb/hr)	(tpy)	Factor
VOC		0.05	8760	0.31	1.34	Gas Analysis
n-Hexane	7.80E-02			0.02	0.10	HYSYS % of VOC
Benzene	1.70E-04			0.00	0.00	HYSYS % of VOC
Toluene	7.23E-04			0.00	0.00	HYSYS % of VOC
Ethylbenzene	9.26E-05			0.00	0.00	HYSYS % of VOC
Xylenes	6.95E-04			0.00	0.00	HYSYS % of VOC
Total HAPs	7.34E-02		8760	0.02	0.11	HYSYS % of VOC
CH4	5.40E+00			1.66	7.25	HYSYS % of VOC

Potential Emissions 11S-LC1-16

Potential Emissions	118-LC1-16					
Pollutant		Emission	Hrs of	Estimated Emis	ssions	Source of
		Factor	Operation			Emission
	% of VOC	(lb/SCF)	(hrs/yr)	(lb/hr)	(tpy)	Factor
VOC	-	0.05	8760	0.01	0.06	Gas Analysis
n-Hexane	7.80E-02			0.19	0.00	HYSYS % of VOC
Benzene	1.70E-04			0.00	0.00	HYSYS % of VOC
Toluene	7.23E-04			0.00	0.00	HYSYS % of VOC
Ethylbenzene	9.26E-05			0.00	0.00	HYSYS % of VOC
Xylenes	6.95E-04			0.00	0.00	HYSYS % of VOC
Total HAPs	7.34E-02		8760	0.20	0.00	HYSYS % of VOC
CH4	5.40E+00			0.07	0.32	HYSYS % of VOC

Noble Energy, Inc. SHL 22 Production Facility

FESCO, Ltd.

1100 Fesco Ave. - Alice, Texas 78332

For: Noble Energy, Inc. 1625 Broadway, Suite 2200 Denver, Colorado 80202

Sample: Sand Hill 8J

Gas Liberated from Separator Water From 560 psig & 70 °F to 0 psig & 70 °F

Date Sampled: 05/08/2014 Job Number: 43289.011

#### CHROMATOGRAPH EXTENDED ANALYSIS - SUMMATION REPORT - GPA 2286

COMPONENT	MOL %		GPM
Hydrogen Sulfide*	0.004	#	
Nitrogen		#	
Carbon Dioxide	1.868		
Methane		#	
Ethane		#	2.744
Propane	1.849		0.513
Isobutane	0.214		0.071
n-Butane	0.477		0.152
2-2 Dimethylpropane	0.000		0.000
Isopentane	0.221		0.081
n-Pentane	0.186		0.068
Hexanes	0.450		0.187
Heptanes Plus	1.037		0.470
Totals		# #	4.286

#### Computed Real Characteristics Of Heptanes Plus:

Specific Gravity 3.650 (Air=1) Molecular Weight 105.41

Gross Heating Value 5592 BTU/CF

#### Computed Real Characteristics Of Total Sample:

Specific Gravity 0.757 (Air=1)
Compressibility (Z) 0.9970
Molecular Weight 21.85
Gross Heating Value
Dry Basis 1069 BTU/CF
Saturated Basis 1051 BTU/CF

\*Hydrogen Sulfide tested in laboratory by: Stained Tube Method (GPA 2377)

Results: <0.013 Gr/100 CF, <0.2 PPMV or <0.001 Mol %

Base Conditions: 14.850 PSI & 60 Deg F

Certified: FESCO, Ltd. - Alice, Texas

Analyst: MR Processor: djv

Cylinder ID: WF-2s David Dannhaus 361-661-7015

Page 1 of 2

FESCO, Ltd.

# CHROMATOGRAPH EXTENDED ANALYSIS TOTAL REPORT - GPA 2286

COMPONENT	МО	GPM	WT %
	L %	Grivi	
Hydrogen Sulfide*	< 0.001		< 0.001
Nitrogen	13.188		16.907
Carbon Dioxide	1.868		3.762
Methane	70.329		51.632
Ethane	10.181	2.744	14.009
Propane	1.849	0.513	3.731
Isobutane	0.214	0.071	0.569
n-Butane	0.477	0.152	1.269
2,2 Dimethylpropane	0.000	0.000	0.000
Isopentane	0.221	0.081	0.730
n-Pentane	0.186	0.068	0.614
2,2 Dimethylbutane	0.018	0.008	0.071
Cyclopentane	0.000	0.000	0.000
2,3 Dimethylbutane	0.029	0.012	0.114
2 Methylpentane	0.131	0.055	0.517
3 Methylpentane	0.089	0.037	0.351
n-Hexane	0.183	0.076	0.722
Methylcyclopentane	0.020	0.007	0.077
Benzene	0.025	0.007	0.089
Cyclohexane	0.033	0.011	0.127
2-Methylhexane	0.085	0.040	0.390
3-Methylhexane	0.088	0.040	0.404
2,2,4 Trimethylpentane	0.000	0.000	0.000
Other C7's	0.082	0.036	0.372
n-Heptane	0.125	0.058	0.573
Methylcyclohexane	0.092	0.037	0.413
Toluene	0.042	0.014	0.177
Other C8's	0.203	0.095	1.024
n-Octane	0.066	0.034	0.345
Ethylbenzene	0.002	0.001	0.010
M & P Xylenes	0.026	0.010	0.126
O-Xvlene	0.003	0.001	0.015
Other C9's	0.095	0.049	0.549
n-Nonane	0.020	0.011	0.117
Other C10's	0.026	0.015	0.168
n-Decane	0.004	0.002	0.026
Undecanes (11)	0.000	0.000	0.000
Totals	100.000	4.286	100.000

#### Computed Real Characteristics Of Total Sample:

Specific Gravity 0.757 (Air=1)
Compressibility (Z) 0.9970
Molecular Weight 21.85
Gross Heating Value
Dry Basis 1069 BTU/CF
Saturated Basis 1051 BTU/CF

Noble Energy, Inc. 5Ht 22 Production Facility

	Stream #	1	2	3	4	2
	Description	Well Fluid to Sand Separator	Well Fluid to GPU Separator	Produced Gas to Sales Pipeline	Water to Tanks	Condensate to Pipeline
	Unit					
Vapor Fraction		0.750	0.738	1.000	0.000	0.000
emperature	F	79.1	70.0	70.0	70.0	70.0
Pressure	psig	2000	500	200	500	200
Vapor Flow	MMSCFD	36.058	36.058	26.610	1	•
Mass Flow	1b/hr	143349	143349	56726	81628	4996
Liquid Flow	barrel/day	17938	17938	11788	2600	550
			Component Mass Fractions	ns		
Methane		0.4977	0.4977	0.6916	0.0000	0.0335
Ethane		0.1257	0.1257	0.1719	0.0000	0.0394
Propane		0.0488	0.0488	0.0640	0.0000	0.0461
i-Butane		0.0089	0.0089	0.0108	0,0000	0.0178
n-Butane		0.0176	0.0176	0.0205	0.0000	0.0462
-Pentane		0.0079	0.0079	0.0076	0.0000	0.0388
n-Pentane		0.0121	0.0121	0.0107	0.0000	0.0710
n-Hexane		0.0174	0.0174	0.0092	0.0000	0.1719
n-Heptane		0.0123	0.0123	0.0031	0.0000	0.1590
n-Octane		0.0125	0.0125	0.0013	0.0000	0.1822
n-Nonane		0.0053	0.0053	0.0002	0.000	0.0815
n-Decane		0.0023	0.0023	0.0000	0.0000	0.0359
C10+*		0.0029	0.0029	0.0001	0.000	0.0458
Nitrogen		0.0036	0.0036	0:0020	0.0000	0.0001
C02		0.0018	0.0018	0.0024	0.0000	0.0003
Oxygen		0.0001	0.0001	0.0001	0.0000	0.0000
H2O		0.2209	0.2209	0.0007	1.0000	0.0001
Benzene		0.0001	0.0001	0.0000	0.0000	0.0009
Toluene		0.0005	0.0005	0.0001	0.0000	0.0063
E-Benzene		0.0001	0.0001	0.000	0.0000	0.0017
o-Xylene		0.000	0.000	0.0001	0.000	0.0134
Cyclohexane		0.0007	0.0007	0.0003	0.0000	0.0080



# WHAT IS CATHODIC PROTECTION?

in soil. Gas and oil professionals around the world know that carosition is a real concern. If the countess miles of pipeline were not protected, the threat of lackage or failure would Cathodic Pratection is providing an electrical current to reduce corrosion of metal structures be greatly increased.

Pipeline Safety states that pipelines operating at certain pressures must have cathodic pratecby a natural corrent flaw, which causes pitting that weakens the pipeline and could result in rion installed. In the corrosion process minute the United States, the D.O.T. Office of leakage ar pipeline failure. The installation of a cathodic protection system reduces or elinitmetal particles are carried from the pipeline nates corrosion. Ξ

# ARROW HAS THE ANSWER

The Arrow Engine Company has a solution to the problem of callodic protection for remote cylinder generators "the Arrow GENSET" can the strategically placed along the pipeline, areacture. This process of callodic protection reduces the deterioration of pipelines that generating the E.C. current onto the pipeline site locations along gas pipelines. Acrow single using pipeline natural gas to fuel the GENSET carry millions of cubic feet of gas daily.

DIX V

C-46 GENSET-AC

# CONTINUOUS CATHODIC PROTECTION















Cathodic Protection

Power Source

Volimeter





Anode

				١
del	Output	Engine RPM	Alternatas RPM	Fuel Rec
SET-AC	5kw	700	1800	2.2 MCF
SET-DC	5kw	700	1800	2.2 MCF
SET-AC	7.5kw	909	1800	3.0 MCF
SET-AC	3.5kw	009	1800	4.7 MCF
VSET-AC	25kw	700	1800	8.2 MCF
VSET-AC	38kw	006	006	14,5 MC
SET.AC	A Show	500	1800	15 34 75

Arrew Engine Company 2301 E. Independence Tulsa, OK 74110

Engine Model	Output	Engine RPM	Alternatas RPM	Fuel Requires
C-46 GENSET-AC	5kw	700	1800	2.2 MCF/D
C-46 GENSET-DC	5kw	700	1800	2.2 MCF/D
C-66 GENSET-AC	7.5kw	909	1800	3.0 MCF/D
C-96 GENSET-AC	3.5kw	900	1800	4.7 MCF/D
C-106 GENSET-AC	25kw	700	1800	8.2 MCF/D
C-255 GENSET-AC	38kw	006	006	14.5 MCF/D
L-795 GENSET-AC	45kw	200	1800	15 MCF/D

www.nrewengina.com

Local 918.583.5711 Fax 918.388.3204 Copyright March 2009

800.331.3662 TOIL FREE

# One user of the Arrow GENSET is located near Brookville, Pennsylvania and has 50 percent of the 720 miles of pipeline in this system that requires operation on Unit 1 and commented that in this time not one both had ever been removed from the unit. Operators with the company stated that they have experienced exceptional results from the Arrow GENSET, with negligible down time, initially they used 1/3 of the unit's capacity, and planned to extend the protection range of the unit. A lacation using an Arraw GENSET recorded mare than 66,000 hours of **CURRENTLY IN USE** cathodic protection.

# LEARN MORE

As that eastern United States gas transmission company found, the Arrow GENSET is a quality collection unit for remote areas. For mare information call the Arrow Engine Company Custamer Service Department at 1 800.50 or vital us at www.arrowengine.com; click on the testimonial tob to view user connents about appendiance of the Arrow Slow Speed GENSETS and other Arrow Engine Power Products.

GRKHOSu

# RP250/RP500\*

#### 250/500W NATURAL GAS OR PROPANE FUELED REMOTE POWER SYSTEM









The RP Series of high efficiency, natural gas or propone fueled Remote Power Systems are based on fuel cell technology developed by Acumentrics and is an excellent option for supply of DC Power to several Off Grid application areas:

- Natural Gas Pipeline & Wellhead
   Cathodic Protection
   SCADA
   RCVs
   Chemical Injection Pumps
- Remote Surveillance
   Cameras
   Routers
   Sensors
   Alarm systems
- Chemical Detection Power Gas Analyzers Radiation detectors
- Off Grid Telecom
   Cellular Base stations
   Radio Transmitters
   Microwave Repeaters
- Wind Energy Assessment
   LIDAR
   SODAR
   Meteorological Tower Heating/Lighting

#### Reliable, Low Maintenance Operation

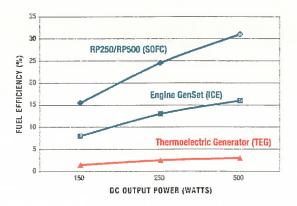
The core of the RP is a solid state, ceramic tubular fuel cell. The system has few moving parts with no motor oil, coolant or hydraulic fluids to change or potentially spill. The system is compact, easy to install. Standard maintenance is an annual site visit to change air and fuel filters. It's scalable and modular so install only as much power as needed, with the option to add more as required.

#### Efficient

The RP fuel cell electrochemically converts a fuel's energy directly into DC electric power. It consumes natural gas or propane, but it does not burn or combust the fuel as in an Internal Combustion Engine (ICE) or a TEG. The combustion process in an ICE or a TEG creates significant waste heat as well as several byproducts that contribute to air pollution. This electrochemical conversion allows the RP to be inherently more efficient than combustion generators so that it can deliver more useable energy from the same amount of fuel. The user benefit is significant fuel/cost savings (see chart below).

#### Whisper Quiet, Clean, Green & Tax Credit Eligible

Unlike loud, noxious engine generators, the RP's virtually sifent fuel cell core enables the direct generation of DC power without emitting NOx and SOx pollutants. RP CO2 emissions are significantly lower than combustion based generators. By switching to an RP from a Thermoelectric Generator (TEG), a user can reduce carbon footprint by up to 50 tons/year or the equivalent of removing 10 cars from the road for a year. Fuel cell products like the RP are defined as renewable energy sources by the US government and are eligible for state and federal tax credits that can be \$3,000 per system or more.





High efficiency RP Power Systems achieve significant fuel savings compared to incumbent technologies.



The Acumentrics RP
Series is a family of quiet,
clean and reliable DC
power systems based on
proprietary tubular ceramic
fuel cell technology to serve
remote or off grid applications.









#### **MODELS** System Options Marie Co. = Auxiliary Output (+12VDC @ max of 100 watts! S Cellular Network Communications -= Satellite Dish Communications = E-Step Butten W H = High Pressure Gas (Allows Max Fuel Infet pressure up to 125psi) - High Sulfur Content Gas W = High Water Content Gas (Recommended for hi water content in gas) SI. Nominal System Output Voltage 12 = 12 VOC 00 24 = 24 VOC48 = 48 VDC September 1 Operating/Control Mode C = Current Control Mode V = Voltage Control Mode B = Battery Charge Mode managg Sanna ( N = illatural Gas (Methane) P = Propane (LP Vapor) 0 Max System DC Gutput Power LO 250 = 250 watts O. \_ 500 = 500 watts U- Base Model

## RP250/RP500\*

#### 250/500W NATURAL GAS OR PROPANE FUELED REMOTE POWER SYSTEM

#### OUTPUT

Fuel Cell Capacity: 500W (RP500) or 250W (RP250) Peak Power from Fuel Cell Bundle

#### **Electrical Efficiency:**

- > 30% @ 500W DC Output Power (RP500)
- > 25% @ 250W DC Output Power (RP250)

DC Output Power: 500W (RP500) or 250W (RP250) Maximum Continuous

DC Output Voltage: User Adjustable, 2-58VDC (RP500), 10-35VDC (RP250)

DC Output Current: 100A Maximum Continuous (RP500), 25A Maximum Continuous (RP250)

Note: Current will also be limited by maximum output power of 500W (RP500) or 250W (RP250)

#### Operating/Control Modes:

Current Control Mode

Voltage Control Mode

Battery Charge Mode

Start-up Time to Max Output Power: <60 minutes

#### FUEL

RP500N or RP250N: Natural Gas RP500P or RP250P: Propane (LP Vapor)

#### Fuel Supply Pressure:

2 to 5 psig for std system;

2 to 125 psig with High Pressure Gas (Option -H)

# Maximum Sulfur Content: <60ppmw (42mg/m3

Maximum Water Content:

#### <5000ppmv for std system;

Solf draining coalescing filter available for

Self draining coalescing filter available for High Water Content Gas (Option -W)

#### **Fuel Consumption:**

@ 500W DC Output Power:

RP500N: 5.70 ft3/hr (0.16 m3/hr) RP500P: 0.06 gals/hr (0.24 liters/hr)

#### @ 250W DC Output Power:

RP250N: 3.51 ft3/hr (0.10 m3/hr) RP250P: 0.04 gals/hr (0.14 liters/hr)

#### **ENVIRONMENTAL**

Operating Temperature:

-40°C to -50°C (-40°F to -122°F)

#### Storage Temperature:

-40°C to -55°C (-40°F to +131°F)

#### Humidity:

5% to 95% (non-condensing))

#### Operating Altitude:

0 to 10,000 ft (3,048m)

#### Storage Altitude:

0 to 40,000 ft (12, 192m)

#### MECHANICAL

#### Nominal Envelope Dimensions (H x W x D):

22in x 22in x 39in (559mm x 559mm x 991mm)

Weight: 300lbs (136kg)

#### COMMUNICATIONS

Local control and monitoring of system status and performance data is standard and can be accessed through an Ethernet cable connection. As an option, the system can also be monitored and controlled remotely.

#### PREVENTIVE MAINTENANCE

Air and fuel filters - Replace annually

Desulfurizer canister - Replace as necessary

Batteries, fans, valves, etc. - Inspect, clean or replace as necessary

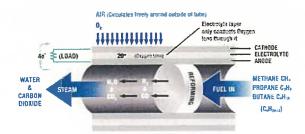
#### WARRANTY

Standard Warranty: 1 year

An extended warranty is available as an option.

#### **SOLID OXIDE FUEL CELL**

SOLID STATE (CERAMIC) CONSTRUCTION



Acumentrics' tubular SOFC technology enables clean, reliable power for your off grid applications.



- Continuous Power for Remote or Off Grid Applications
- High Energy Efficiency Yields Significant Fuel Savings
- Available Fuel Options Natural Gas & Propane
- Low Maintenance Solid State Construction
- Safe, Quiet and Clean Electrochemical Fuel Conversion Minimizes Emissions

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20 Southwest Park • Westwood, MA 02090
Tel: 800-332-0277 • FAX: 781-461-1261
www.acumentrics.com\fuel-cell-generators.html

# DATA SHEET Specifications & Performance

#### **Certified Quality**







Quality System
ISO 9001 Certified



Environmental Management System ISO 14001 Certified





Certified to CSA Technical Letter No. R-14



Certified to ANSI LC6-2008



Warren Rupp, Inc. A Unit of IDEX Corporation 800 N. Main St., Mansfield, Ohio 44902 USA Telephone 419.524.8388 Fax 419.522.7867 SANDPIPERPUMP.COM

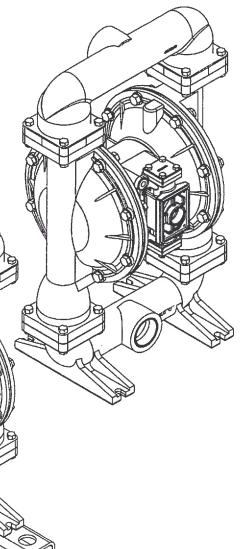


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# **Model G20**

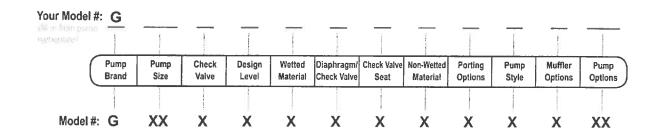
Metallic Design Level 1

Natural Gas-Operated Diaphragm Pumps





# **Explanation of Pump Nomenclature**



#### **Pump Brand**

G Gas Operated

#### **Pump Size**

#### **Check Valve Type**

B Ball

#### Design Level

Design Level

#### **Wetted Material**

- Stainless Steel
- A Aluminum

#### **Diaphragm/Check Valve Materials**

- B Nitrile/Nitrile
- V FKM / FKM
- 5 Nitrile/PTFE

#### **Check Valve Seat**

Stainless Steel

- B Nitrile
- PTFE
- Aluminum

#### **Non-Wetted Material Options**

- Painted Aluminum
- Unpainted Aluminum with Stainless Steel Gas Valve
- Unpainted Aluminum with Stainless Steel Gas Valve with FKM O-rings
- Unpainted Aluminum
- Unpainted Aluminum/FKM Elastomers
- Unpainted Aluminum/FKM Elastomers
- Stainless Steel/ S02/304 SS Hardware
- Stainless Steel/ 316 Stainless Hardware
- Painted Stainless Steel
- Stainless Steel/FKM Elastomers
- Painted Stainless Steel/FKM Elastomers

#### **Porting Options**

- NPT Threads
- BSP (Tapered) Threads
- 150# Raised Face 2" ANSI Flange w/ Threaded Pipe Connections
- 150# Welded Raised Face 2" ANSI Flanged Manifolds

#### **Pump Style**

Standard

#### **Muffler Options**

X No Muffler Permitted \*

### **ATEX Detail**

 ATEX Rating	Wetted Material Options	Non-Wetted Material Options
II 1G c T5 II 1D c T100°C I M1 c I M2 c	S	S, T, 7, 8, 9
II 2G c T5 II 2D c T100°C	All Options	All Options

## **Performance**

#### **G20 METALLIC**

SUCTION/DISCHARGE PORT SIZE

• 2"

#### CAPACITY

 0 to 150 gallons per minute (0 to 567 liters per minute)

#### **GAS DISTRIBUTION VALVE**

No-lube, no-stall design

#### **SOLIDS-HANDLING**

• Up to .25 in. (6mm)

#### **HEADS UP TO**

 100 psi or 231 ft, of water (7 bar or 70 meters)

#### **MAXIMUM OPERATING PRESSURE**

• 100 psi (7 bar)

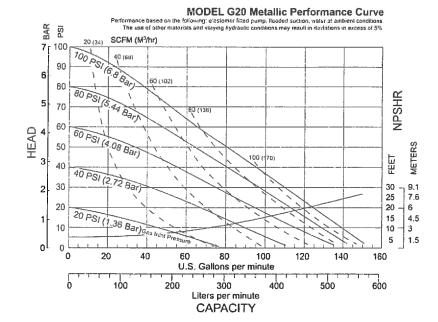
#### **DISPLACEMENT/STROKE**

.42 Gallon / 1.59 liter

#### **SHIPPING WEIGHT**

- · Aluminum 69 lbs. (31kg)
- · Stainless Steel 114 lbs. (52kg)

These pump models are designed to pump the following fluids: Crude Cil. Salt Water, Drilling Mud, Condensate, Lubrication Oils, Glycol, Caustic Liquids, and Acids."



Exhaust Gas: The exhausted natural gas must be vented to a low pressure safe location in accordance with local fire safety and environmental codes, or in the absence of local codes, an industry or nationally recognized code having jurisdiction over the specific installations, and/or CAN/CGA B149, Installation Codes

#### **Materials**

Material Profile:	Operating Temperatures:	
CAUTION! Operating temperature limitations are as follows:	Max.	Min.
FKM: (Fluorocarbon) Shows good resistance to a wide range of oils and solvents; especially all aliphatic, aromatic and halogenated hydrocarbons, acids, animal and vegetable oils. Hot water or hot aqueous solutions (over 70°F(21°C)) will attack FKM.	350°F 177°C	-40°F -40°C
Nitrile: General purpose, oil-resistant. Shows good solvent, oil, water and hydraulic fluid resistance. Should not be used with highly polar solvents like acetone and MEK, ozone, chlorinated hydrocarbons and nitro hydrocarbons.	190°F 88°C	-10°F -23°C
Virgin PTFE: (PFA/TFE) Chemically inert, virtually impervious. Very few chemicals are known to chemically react with PTFE; molten alkali metals, turbulent liquid or gaseous fluorine and a few fluoro-chemicals such as chlorine trilluoride or oxygen difluoride which readily liberate free fluorine at elevated temperatures.	220°F 104°C	-35°F -37°C

Maximum and Minimum Temperatures are the limits for which these materials can be operated. Temperatures coucled with pressure affect the longevity of diaphragm pump components. Maximum life should not be expected at the extreme limits of the temperature ranges.

#### Metals:

Stainless Steel: Equal to or exceeding ASTM specification A743 CF-8M for corrosion resistant iron chromium, iron chromium nickel and nickel based alloy castings for general applications. Commonly referred to as 316 Stainless Steel in the pump industry.

For specific applications, always consult the Chemical Resistance Chart

Ambient temperature range:

-20°C to +40°C

Process temperature range:

-20°C to +30°C for models rated as category 1 equipment

-20°C to +30°C for models rated as category 1 equipment -20°C to +100°C for models rated as category 2 equipment

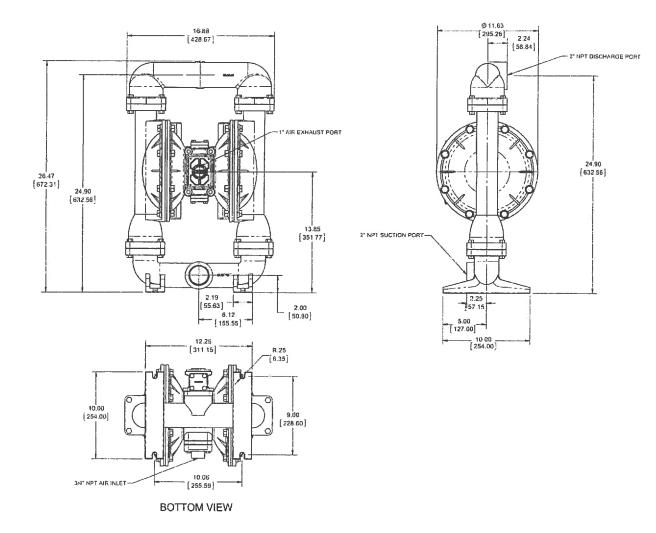
In addition, the ambient temperature range and the process temperature range do not exceed the operating temperature range of the applied non-metailic parts as listed in the manuais of the pumps



# **Dimensional Drawings**

#### **G20 Metallic**

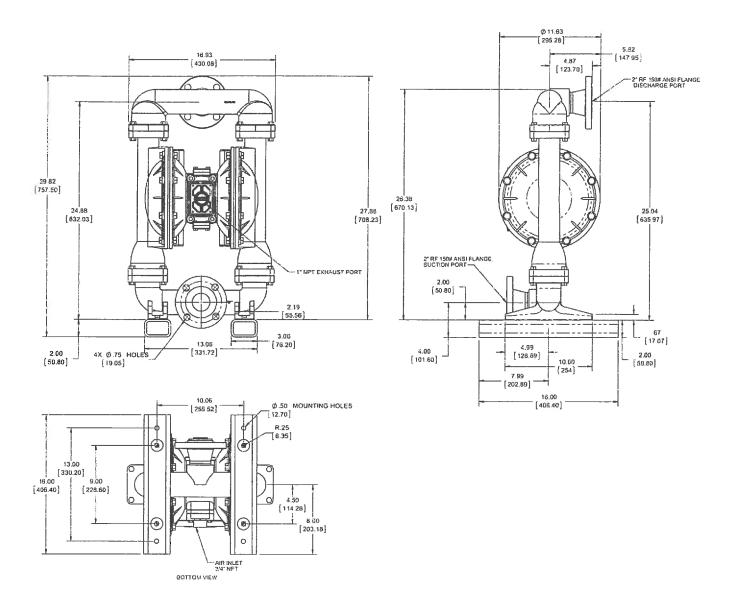
Dimensions in inches (mm dimensions in brackets). Dimensional Tolerance:±1/8" (± 3mm)
The dimensions on this drawing are for reference only. A certified drawing can be requested if physical dimensions are needed.



# **Dimensional Drawings**

#### **G20 Metallic - ANSI Flange**

Dimensions in inches (mm dimensions in brackets). Dimensional Tolerance:±1/8" (± 3mm)
The dimensions on this drawing are for reference only. A certified drawing can be requested if physical dimensions are needed



# 5 - YEAR Limited Product Warranty

Warren Rupp, Inc. ("Warren Rupp") warrants to the original end-use purchaser that no product sold by Warren Rupp that bears a Warren Rupp brand shall fail under normal use and service due to a defect in material or workmanship within five years from the date of shipment from Warren Rupp's factory. Warren Rupp brands include Warren Rupp®,SANDPIPER®, MARATHON®, PortaPump®, SludgeMaster™ and Tranquilizer®.

~ See sandpiperpump.com/content/warranty-certifications for complete warranty, including terms and conditions, limitations and exclusions. ~

#### WARREN RUPP, INC.

# **Declaration of Conformity**

Manufacturer: Warren Rupp, Inc., 800 N. Main Street Mansfield, Ohio, 44902 USA

Certifies that Air-Operated Double Diaphragm Pump Series: HDB, HDF, M Non-Metallic, S Non-Metallic, M Metallic, S Metallic, T Series, G Series, U Series, EH and SH High Pressure, RS Series, W Series, SMA and SPA Submersibles, and Tranquilizer® Surge Suppressors comply with the European Community Directive 2006/42/EC on Machinery, according to Annex VIII. This product has used Harmonized Standard EN809:1998+A1:2009, Pumps and Pump Units for Liquids - Common Safety Requirements, to verify conformance.

David Reseberry
Signature of authorized person

David Roseberry
Printed name of authorized person

Revision Level: F

October 20, 2005

Date of issue

Engineering Manager

Title

August 23, 2012

Date of revision





# WARREN RUPP, INC.

# **EC / EU Declaration of Conformity**

The objective of the declaration described is in conformity with the relevant Union harmonisation legislation: Directive 94/9/EC (until April 19, 2016) and Directive 2014/34/EU (from April 20, 2016).

#### Manufacturer:

Warren Rupp, Inc. A Unit of IDEX Corportion 800 North Main Street P.O. Box 1568 Mansfield, OH 44902 USA

#### Applicable Standard:

EN13463-1: 2001 EN13463-5: 2003 EN60079-25: 2004

#### Harmonised Standard:

EN13463-1: 2009 EN13463-5: 2011 EN60079-25:2010

The harmonised standards have been compared to the applicable standards used for certification purposes and no changes in the state of the art technical knowledge apply to the listed equipment.

#### **AODD Pumps and Surge Suppressors**

Technical File No.: 203104000-1410/MER

#### AODD (Air-Operated Double Diaphragm) Pumps

EC Type Examination Certificate No. Pumps: KEMA 09ATEX0071 X

DEKRA Certification B.V. (0344) Meander 1051 6825 MJ Arnhem The Netherlands

#### **Hazardous Locations Applied:**



**Tranquilizer®** 

DATE/APPROVAL/TITLE: 18 March 2016

David Roseberry, Director of Engineering



Noble Energy, Inc. SHL 22 Production Facility

#### ATTACHMENT P

Class I Legal Advertisement

# AIR QUALITY PERMIT NOTICE Notice of Application for Permit Application

Notice is given that Noble Energy, Inc. has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a 45CSR13 Permit for its SHL 22 oil and natural gas production facility located in Marshall County West Virginia at latitude 39.99576622 and longitude -80.56099553. From Interstate 70, take Dallas Pike Road Exit (Exit 11), at bottom of ramp, make a right if traveling east or left if traveling west onto CR 41 (Dallas Pike Road), and travel Dallas Pike Road approximately 4.9 miles to the town of Dallas, make a right onto CR 7 (Stone Church/Sand Hill Road), make a right onto Stone Church/Sand Hill Road and travel approximately 1.8 miles to CR 7 (Wye Intersection) – Sand Hill Road, make a left hand turn onto Sand Hill Road and travel approximately 1.1 miles to CR 9 - Standiford Hill Road, make a right turn onto Standiford Hill Road and travel 0.1 mile to lease road on left.

The applicant estimates the potential to discharge the following Regulated Air Pollutants will be:

Regulated Pollutant	Potential Annual Emissions in tons per year (tpy)	
Carbon Monoxide	30.67	
Nitrogen Oxides	11.34	
Particulate Matter (PM)	0.47	
PM-10	0.47	
Sulfur Dioxide	0.04	
Total Volatile Organic Compounds	26.51	
Total Hazardous Air Pollutants	2.44	
Total Carbon Dioxide Equivalent	17,363	

Startup of the operation is planned to begin on or about February 22, 2017. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this application for 45CSR13 Permit should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours.

Dated this,

Thursday, October 06, 2016

Ву:

Noble Energy, Inc.

**RJ Moses** 

Operations Manager Marcellus Business Unit 1000 Noble Energy Drive Canonsburg, PA 15317